

Development of Fission Gas and Species Transport Capabilities in SAM

Bob Salko, Davide Rotilio, Xingang Zhao, Travis Mui, Rui Hu

Molten Salt Reactor Program Annual Review

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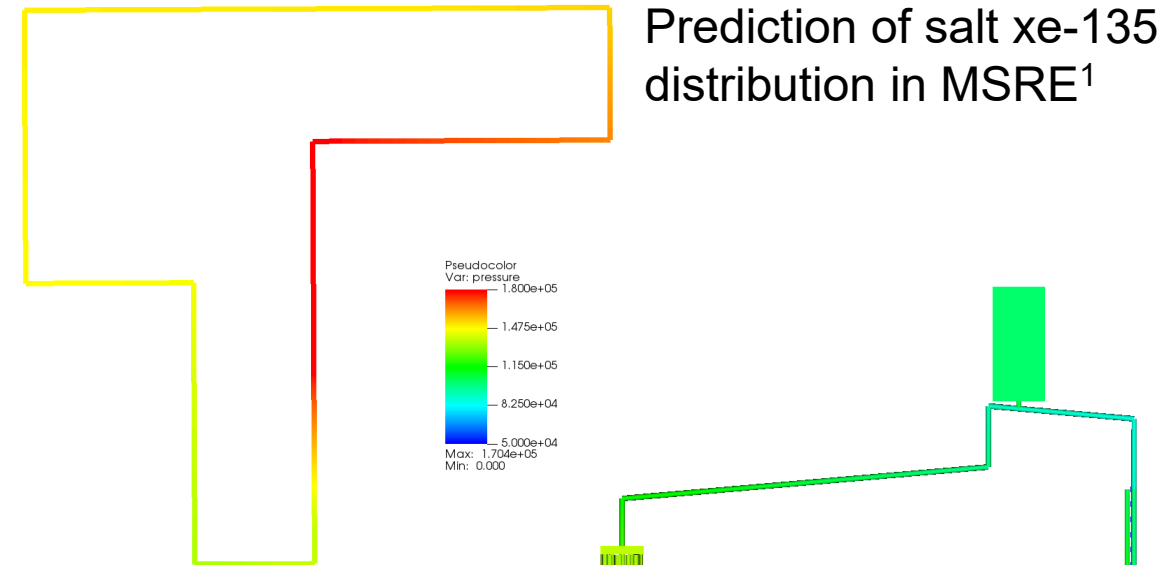
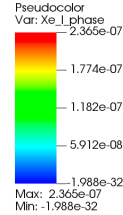


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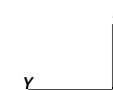
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Introduction

- A modern system analysis code for advanced non-LWR safety analysis
 - Covers almost all non-LWR concepts
- Ongoing efforts to develop SAM for MSR applications
 - Salt thermophysical properties
 - Salt freezing
 - Species tracking for delayed neutron precursors and fission products in both salt and sparge gas
 - Species decay and decay heat
 - Species phase transfer
 - Modeling of non-condensable gas transport
- Validation using MSRE, MSR Campaign data, and open two-phase data



Prediction of pressure distribution in LSTL²

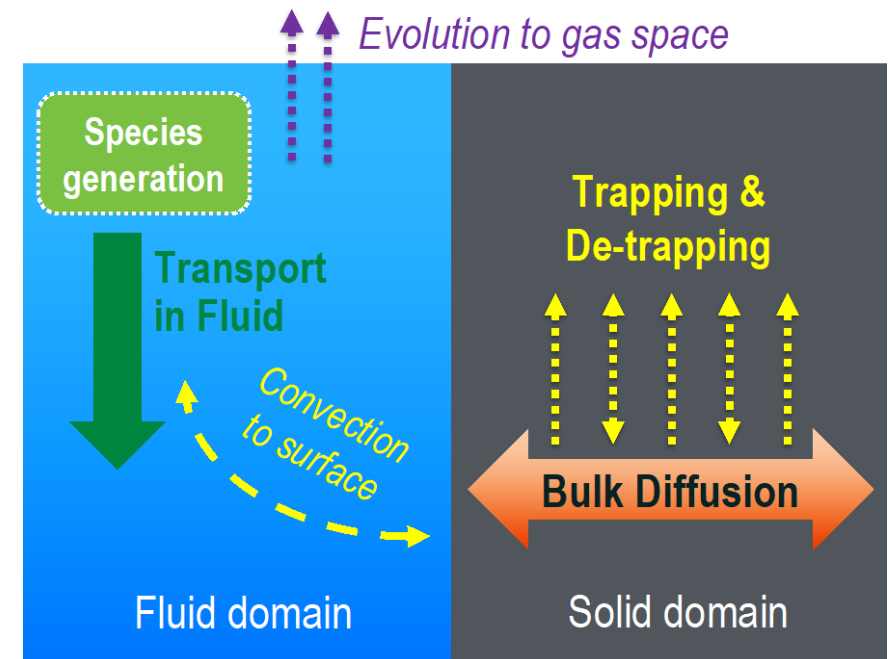


Prediction of salt xe-135 distribution in MSRE¹



Species Tracking in SAM

- Generic species (passive scalar) transport originally implemented in SAM to model flowing delayed neutron precursors in MSRs
- Framework expanded to simulate transport pathways of tritium in FHRs and MSRs
 - Collaboration with T. Fuerst on MSTTE modeling
- Ongoing work to consider additional applications:
 - Oxidation-corrosion in lead-cooled reactors
 - Redox corrosion in salt-cooled reactors
 - Noble gas/metal transport in MSR

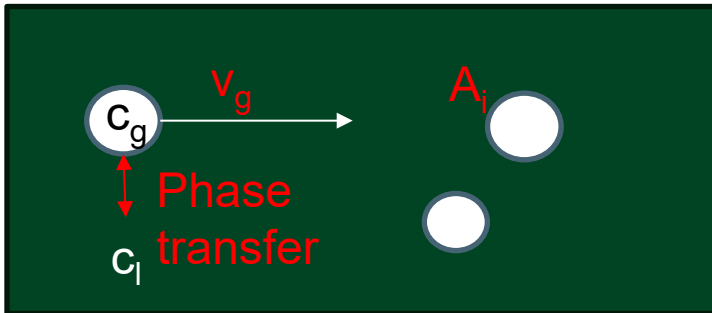


Species transport pathways modeled in SAM



Enhancements to Species Tracking

- Species can now exist in the gas phase
 - Transported by gas velocity
- Phase transfer using Henry's Law for high-volatile gas
 - Henry and mass transfer coefficient calculated by Mole
 - Interfacial area and gas velocity by SAM
- Capture decay between species



Iodine transport in liquid

$$\frac{\partial I_l}{\partial t} + \frac{\partial (v_l I_l)}{\partial x} = -\lambda_I I_l + \gamma_I \bar{\Sigma}_f \Phi_f$$

Xenon transport in liquid

$$\frac{\partial X_{e_l}}{\partial t} + \frac{\partial (v_l X_{e_l})}{\partial x} = -\lambda_{Xe} X_{e_l} + \lambda_l I_l - \underbrace{K_l A_i (X_{e_g} HRT - X_{e_l})}_{\text{Added phase transfer term}}$$

Xenon transport in gas

$$\frac{\partial X_{e_g}}{\partial t} + \frac{\partial (v_g X_{e_g})}{\partial x} = -\lambda_{Xe} X_{e_g} + \underbrace{K_l A_i (X_{e_g} HRT - X_{e_l})}_{\text{Added phase transfer term}}$$

Species can exist in gas phase

Track decay from one species to another

Mass transfer data from Mole

Added phase transfer term

Gas/bubble behavior predicted by SAM

c : Species concentration (mol/m³)
 v : Species velocity (m/s)
 λ : Species decay coefficient (1/s)
 l/g : Liquid/gas phase index

I : Iodine concentration (#/m³)
 Xe : Xenon concentration (#/m³)
 A_i : Interfacial area (m²/m³)

K_l : Mass transfer coefficient (m/s)
 H : Henry's coefficient (mol/m³/atm)
 R : Universal gas constant (J/mol/K)
 T : Temperature (K)



Coupling to Saline and Mole

- Mole provides modeling of high-volatile species phase transfer¹
 - Utilizes two-film theory
 - Provides Henry coefficients for FLiNaK and FLiBe salts and several noble gases
 - Mass transfer coefficient determined using Wilke-Chang or Stokes-Einstein¹
- Saline is a C++/Fortran/Python interface to MSTDB-TP
 - Integrated into MOOSE and SAM
 - Provides thermophysical properties of many common salts and salt compositions

Bulk Gas	Gas Film	Liquid Film	Bulk Liquid
p_i pressure	p_i^*	c_i^*	c_i concentration

$$c_i^* = p_i H$$

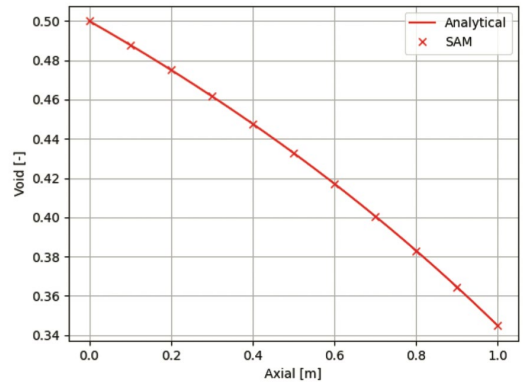
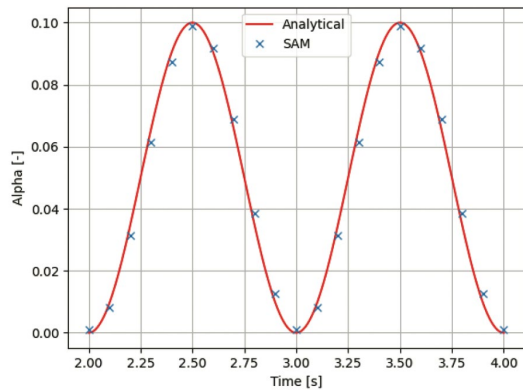
$$p_i^* = c_i / H$$

Gas liquid interface modeled using two-film theory

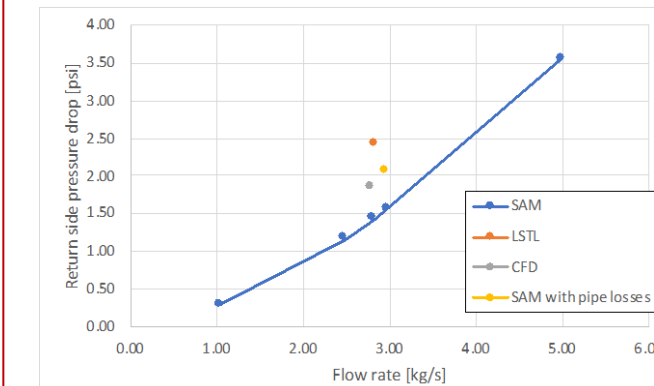
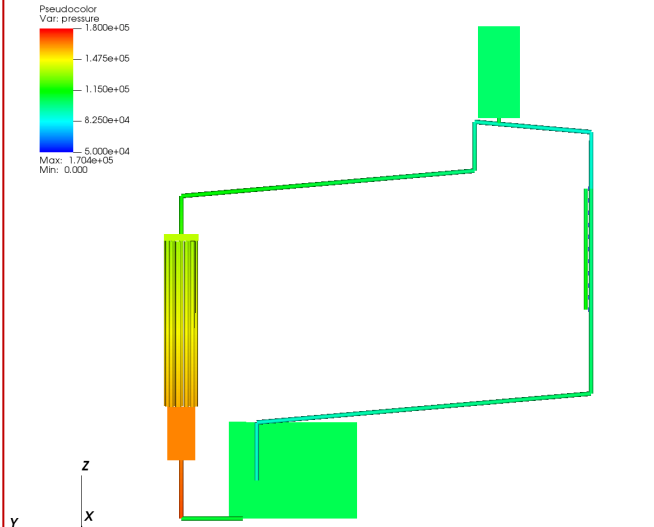
$$\Phi_j = K_j^L (p_j^g H_j - c_j^l) = K_j^G (p_j^g - c_j^l / H)$$

Interface concentrations determined using Henry's Law

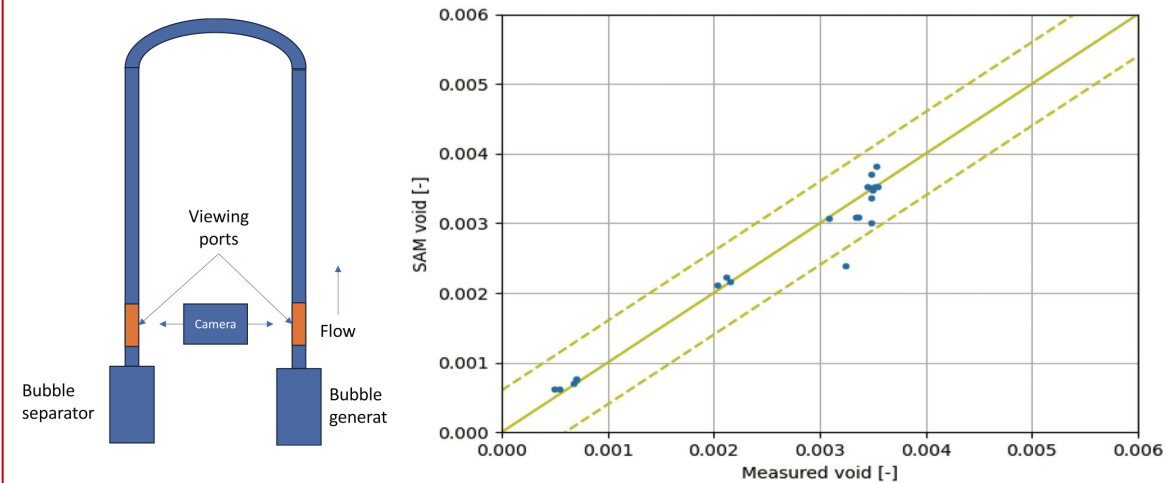
Verification and Validation Activities



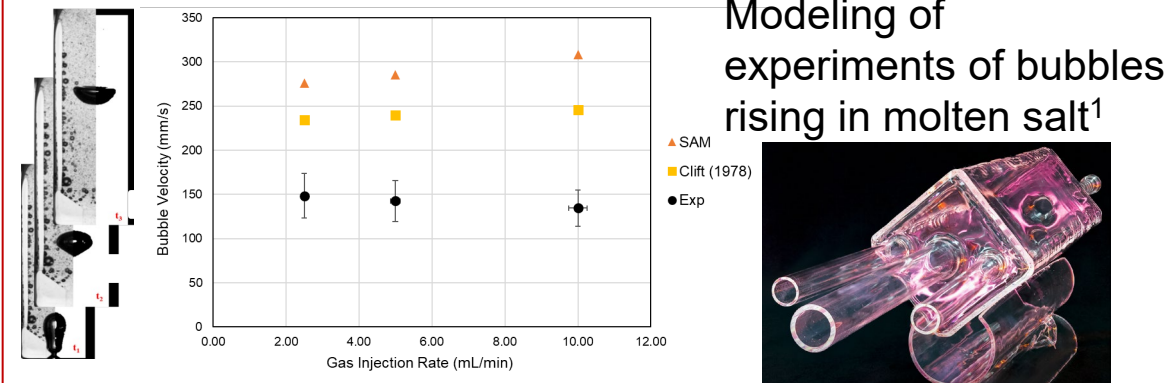
Development of verification test suite for gas transport model³



Modeling of pressure drop in LSTL²



Modeling of void fraction in Kress experiment³

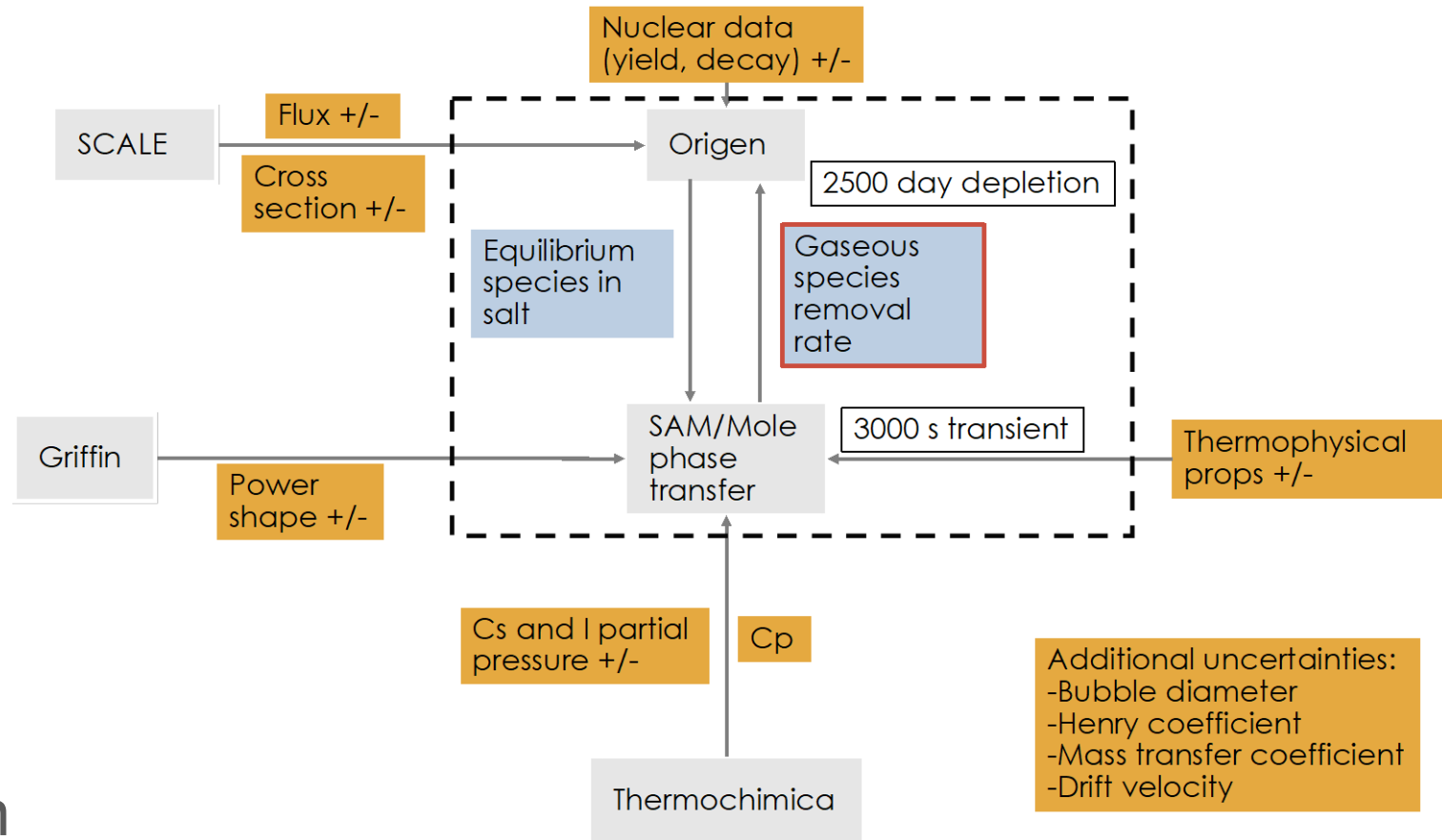


Modeling of experiments of bubbles rising in molten salt¹

1. McFarlane, J., et al. "Design of Instrumentation for Noble Gas Transport in LSTL Needed for Model Development" Report. ORNL TM-2023-3138 (2023).
2. Yoder, G., et al. "Development of a forced-convection liquid-fluoride-salt test loop", Proceedings of HTR, 2010
3. Salko, R, et al. "Implementation of a Drift Flux Model into SAM with Development of a Verification and Validation Test Suite for Modeling of Noncondensable Gas Mixtures", Nuclear Technology. 2024

Modeling of Off-Gas System

- Model pool-type MSR
 - Bubble generation due to xenon creation and phase transfer
 - Species and bubble transport affects fission gas concentration in pool region
 - Bubble buoyancy leads to escape at pool surface
- Depletion determines fission product inventory



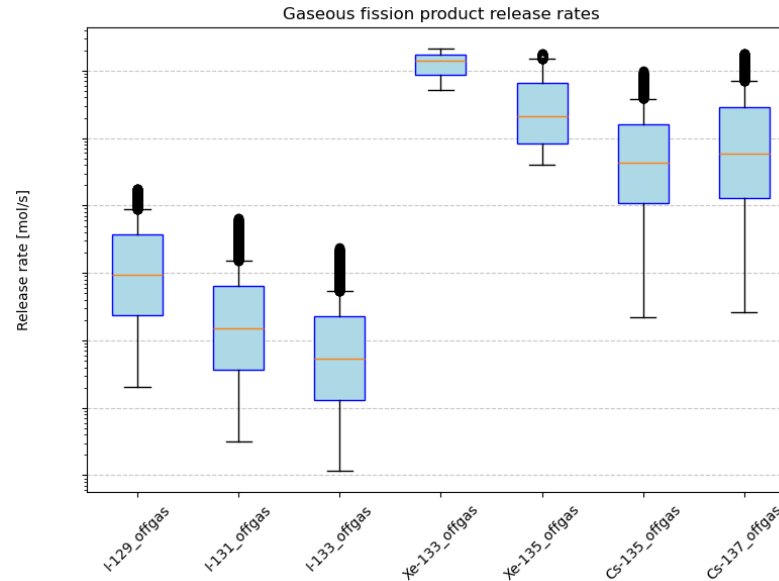
Coupled system being utilized for prediction of off-gas of fission products plus uncertainty¹

1. DOE iFOA project in collaboration with Terrestrial Energy, USA



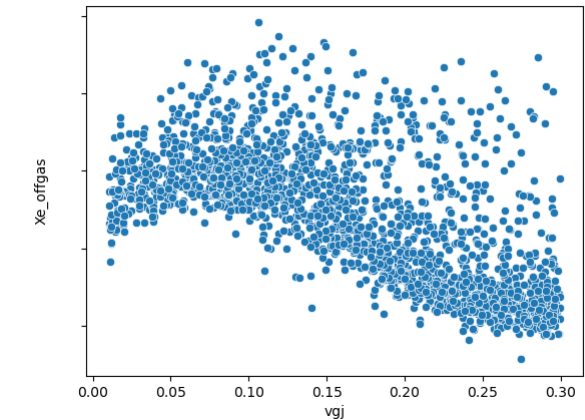
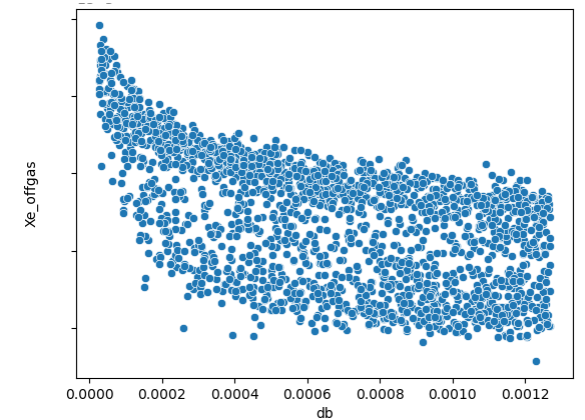
Uncertainty Quantification of Off-gas

- Forward UQ analysis of off-gas modeling
 - Variation of 15 input parameters
 - Nuclear data, thermophysical fluid properties, mass transfer data, bubble behavior
 - Xenon, cesium, and iodine off-gas rate are figures of merit (FOM)
 - 5,000 evaluations of coupled analysis lead to convergence of FOMs
- Bubble velocity uncertainty obtained from MSR Campaign data¹



Spread in off-gas release rates due to input uncertainties

Bubble terminal velocity, bubble diameter, and thermochemical data found to be potentially high importance



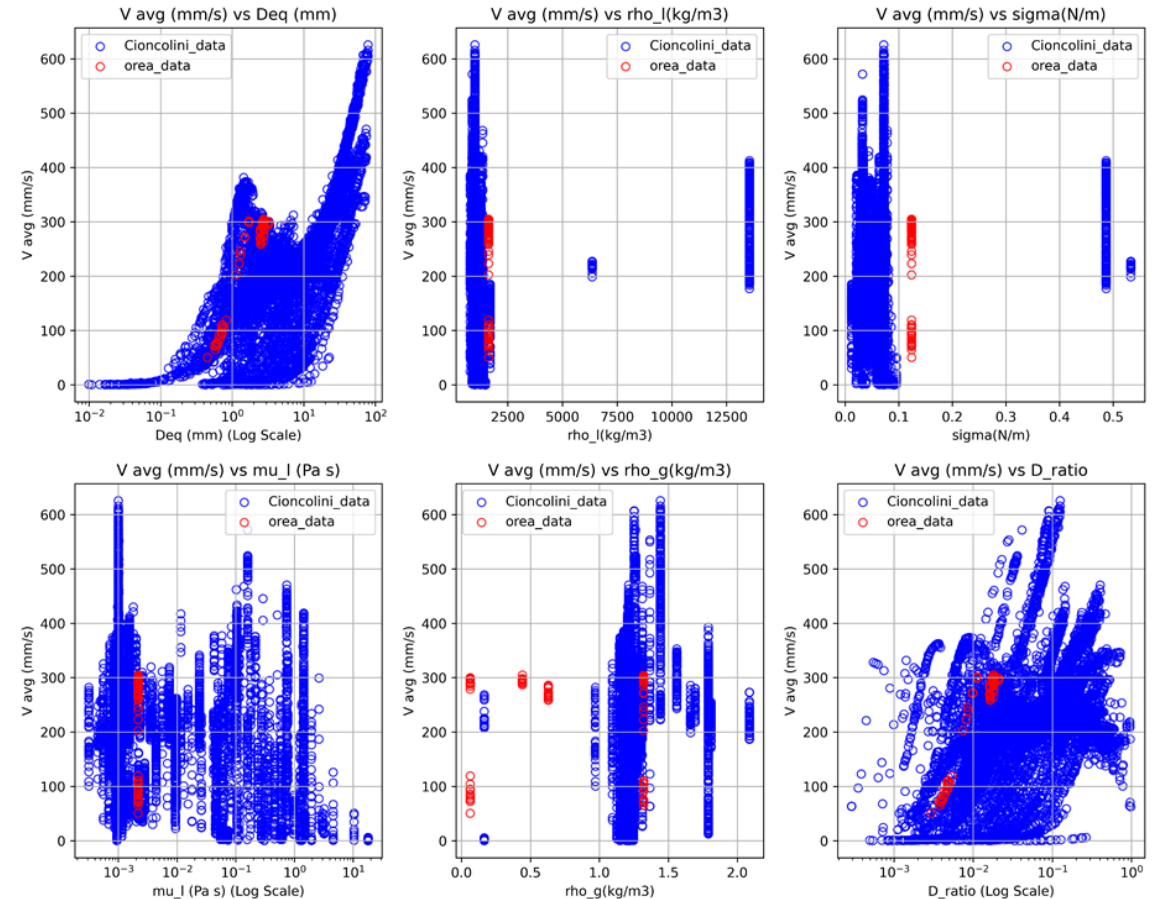
Relationship between input parameters and off-gas rates

1. Daniel Orea, Kevin Robb, Joanna McFarlane, Comparative study between experimental measurements and model predictions of bubble rise velocity in molten LiCl-KCl, Nuclear Engineering and Design, Volume 443, 2025, 14247, ISSN 0029-5493,



SAM Data Needs

- Gas bubble behavior in stagnant and pumped salt systems
 - Bubble coalescence, breakup, interfacial effects on slip and buoyancy
- Mass transfer behavior due to phase change and solid interaction
 - Impact of noble metals
- Salt entrainment and transport at free surfaces

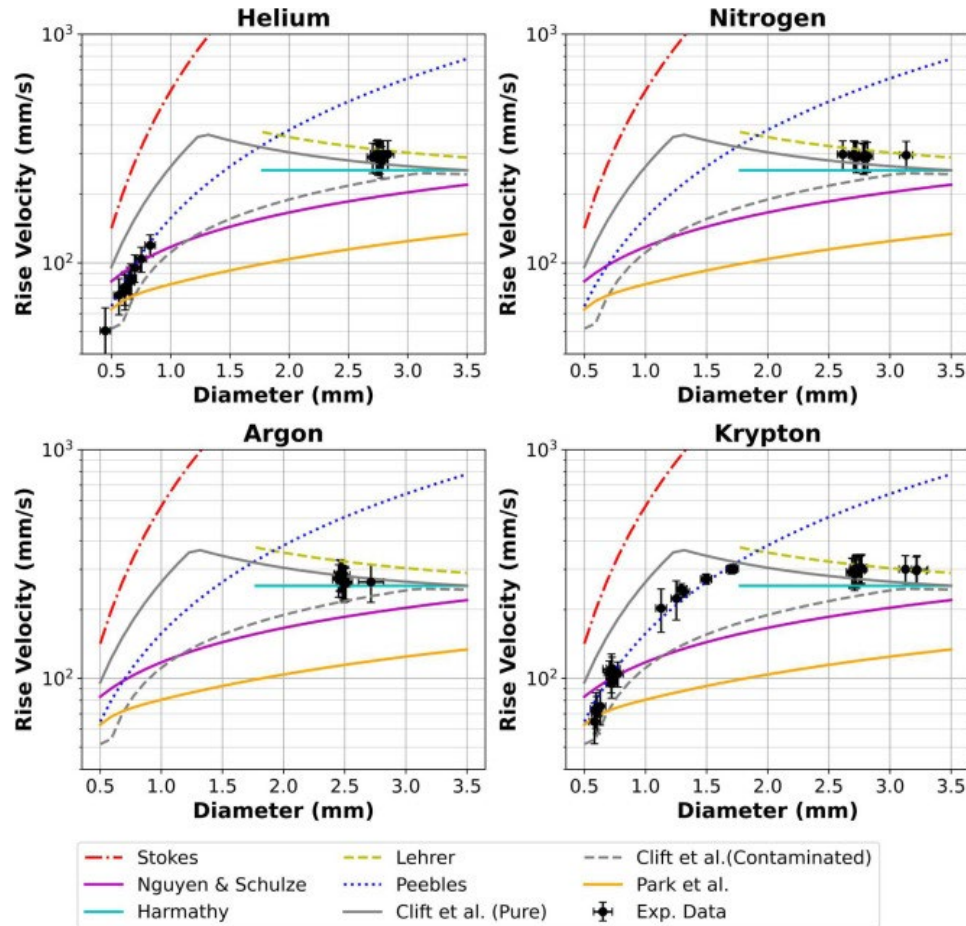


New salt data (red) produced by Orea¹ covers new two-phase conditions and is used for SAM development

1. Daniel Orea, Kevin Robb, Joanna McFarlane, Comparative study between experimental measurements and model predictions of bubble rise velocity in molten LiCl-KCl, Nuclear Engineering and Design, Volume 443, 2025, 14247, ISSN 0029-5493,



Modeling bubble rise in salt



$$\text{Harmathy: } v = 1.53 \left[\frac{\Delta \rho g \sigma}{\rho_l^2} \right]^{0.25} \text{ for } Re > 500$$

Original model implemented in SAM

$$\text{Clift: } \begin{cases} v = 0.138 g^{0.82} \left(\frac{\rho}{\mu} \right)^{0.639} D_{eq}^{1.459} & \text{if } D_{eq} < 1.3 \text{ mm} \\ v = \sqrt{\frac{2.14 \sigma_l}{\rho_l D_{eq}}} + 0.505 g D_{eq} & \text{if } D_{eq} \geq 1.3 \text{ mm} \end{cases}$$

Clift model recognizes bubble size

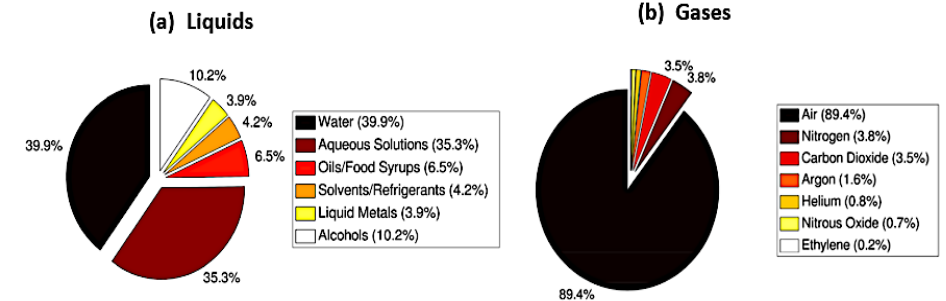
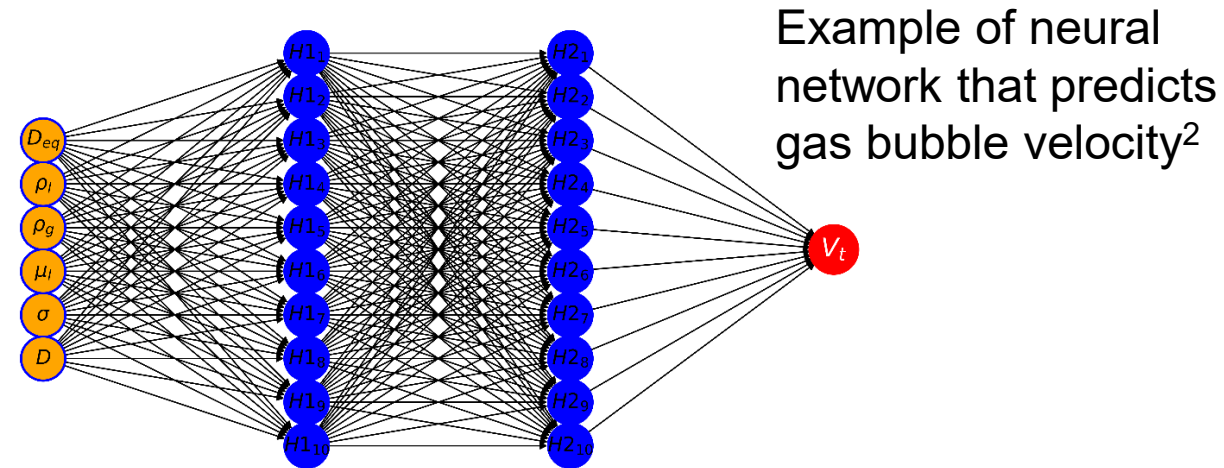
$$\text{DSM Clift } \begin{cases} v = 0.136 g^{0.799} \left(\frac{\rho}{\mu} \right)^{617} D_{eq}^{1.459} & \text{if } D_{eq} < 1.75 \text{ mm} \\ v = \sqrt{\frac{2.366 \sigma_l}{\rho_l D_{eq}}} + 0.566 g D_{eq} & \text{if } D_{eq} \geq 1.75 \text{ mm} \end{cases}$$

Modified form developed by Orea¹

1. Daniel Orea, Kevin Robb, Joanna McFarlane, Comparative study between experimental measurements and model predictions of bubble rise velocity in molten LiCl-KCl, Nuclear Engineering and Design, Volume 443, 2025, 14247, ISSN 0029-5493,

Development of a new model using machine learning

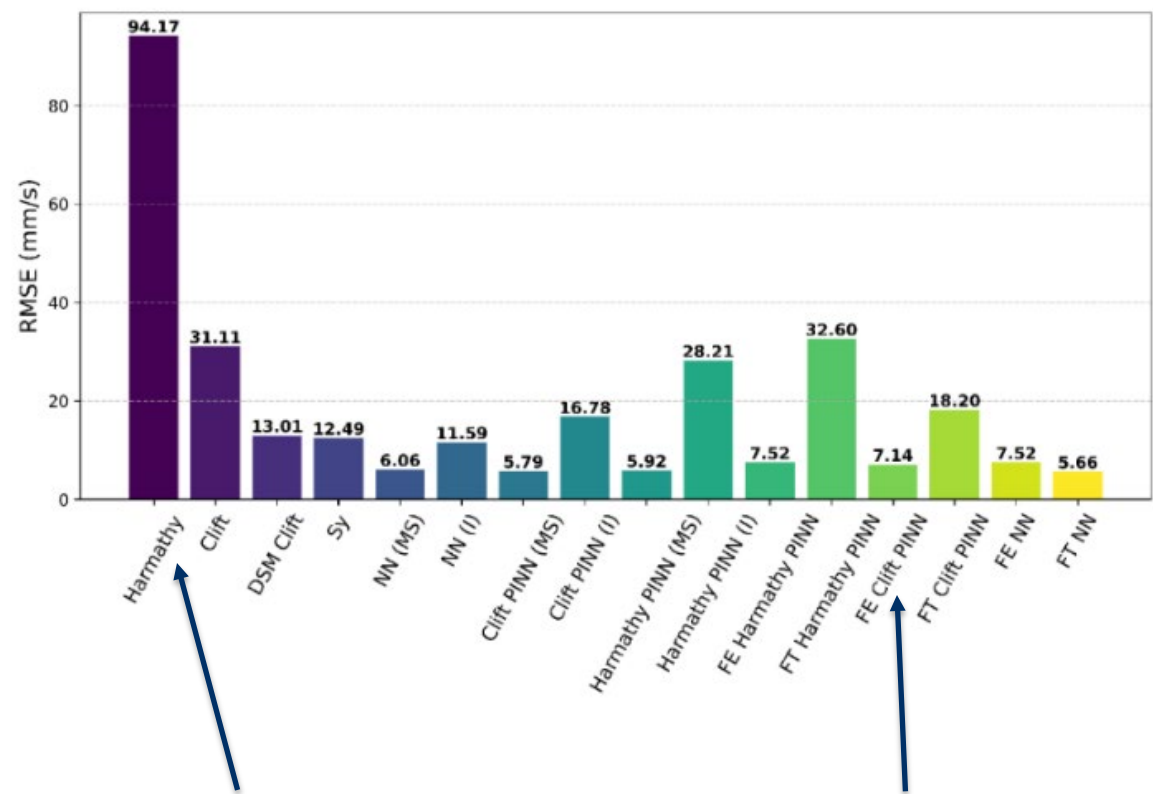
- UTK led efforts to develop an ML model using three approaches:
 - Pure neural network trained on data
 - Physics informed neural network - use existing model to constrain neural network
 - Symbolic regression – discover model form
- Transfer learning techniques tested
 - Start with Cioncolini database¹ (7,000 data points)
 - Fine tune with Orea data
- Model implemented into SAM



Large bubble database (non-salt) used to supplement model training using transfer learning

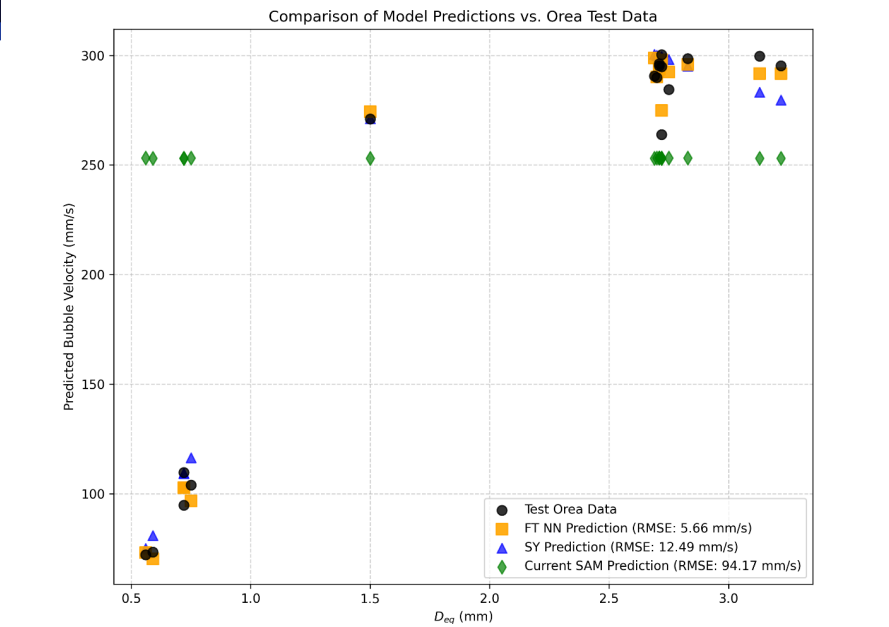
1. Cioncolini, A. and Magnini, M. (2025). Solitary bubbles rising in quiescent liquids: A critical assessment of experimental data and high-fidelity numerical simulations, and performance evaluation of selected prediction methods. *Phys. Fluids*, 37(2), 021304

Development of a new model using machine learning



Existing model performs poorly on Orea data

Both fine tuned NN and fine tuned PINN models perform best



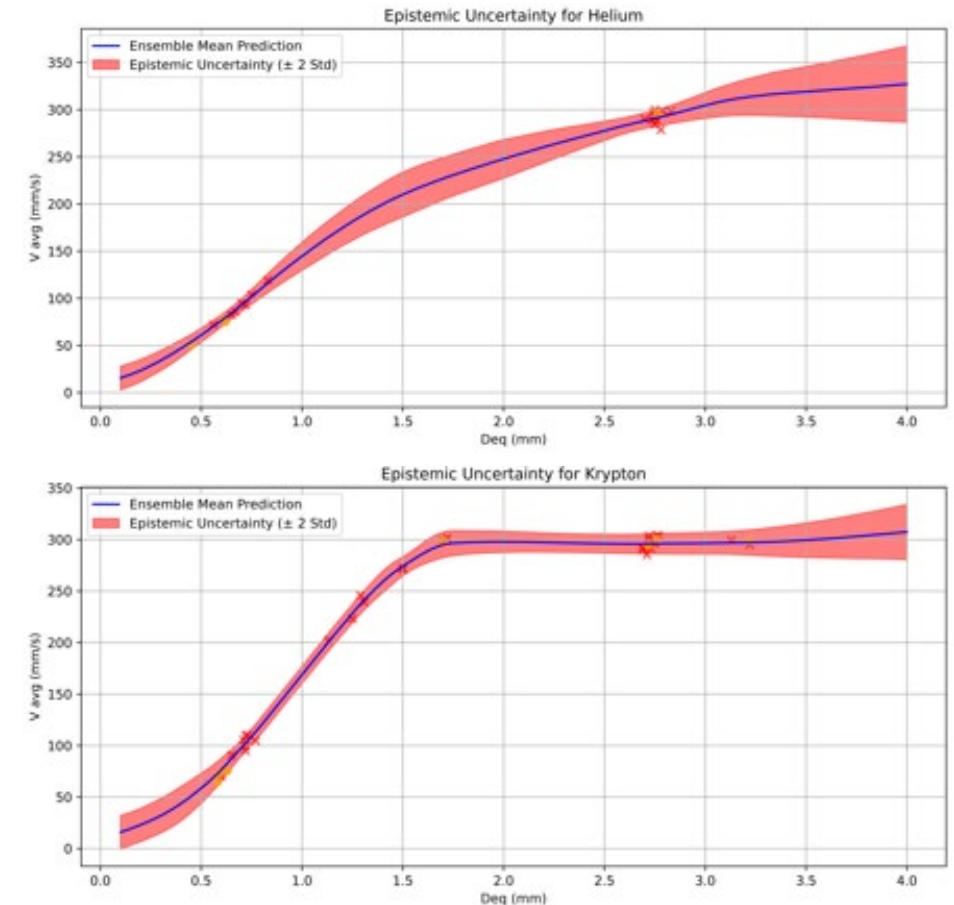
Comparison of models against Orea data

$$V_t = \frac{1.0065 (D_{eq} g)^{0.5}}{\exp\left(\frac{-1.9253}{E_o + \frac{0.11613}{E_o}}\right) + \left(\frac{37.741}{(Oh + 0.44101) * Ar}\right) + 0.37981 + Oh}$$

Symbolic regression model

Including model uncertainty

- Deep ensemble used to quantify ML model uncertainty
 - Train many models with different initialization
 - Identifies epistemic and aleatoric sources of uncertainty
 - Regions of high uncertainty indicate future data needs for high impact model improvements



Model prediction and uncertainty for different bubble sizes can inform future data needs



Summary

- Species and gas transport modeling capabilities expanded in SAM for modeling of MSRs
 - Ability to track gaseous species using drift flux
 - Ability model phase transfer, decay between species, and bubble release
- Demonstration of capabilities shown by performing fission gas release uncertainty analysis
- Model is being expanded including coupling with Thermochemica, bubble modeling improvements based on MSR Campaign data, graphite xenon absorption, and improved coupling for depletion
- Future work on salt spill, improvements on noble gas and noble metal transport, and continued collaboration with MSTTE campaign
- Additional data in high uncertainty regions will improve model accuracy and uncertainty





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Enhancements to Species Tracking

- Mass transfer correlations developed from high-fidelity MOSCATO/NekRS¹ have been integrated into SAM
- Porous diffusion of species in solids also modeled (e.g. Xe in graphite)
 - Dissolved fluid species transfers to graphite pore space through a two-film model
 - Knudsen diffusion within pore gas space
- Species reactivity feedback added to PKE model to account for evolution of Xe-135 concentration
 - Reactivity feedback will integrate provided reactivity coefficients with species concentrations and volume over axial length for gas/liq/solid phase
 - Integrated into SAM Point Kinetics model, work is ongoing to demonstrate using MSRE

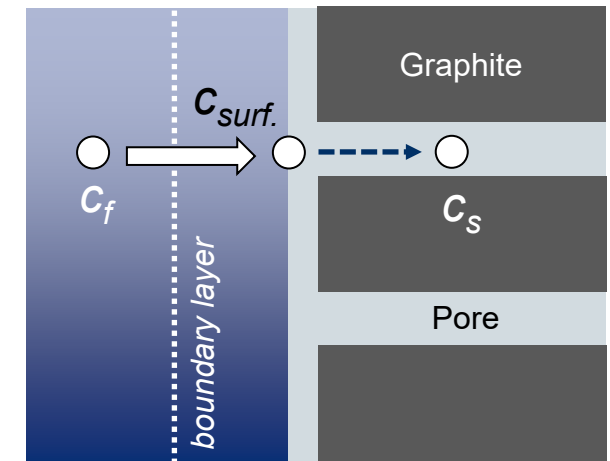
Species porous diffusion in solids (Xenon in graphite)

$$\frac{\partial c_s}{\partial t} - \frac{D_{Xe,s}}{\varepsilon} (\nabla^2 c_s) - \lambda_{Xe} c_s = 0$$

Fluid-solid interface species flux

$$J_{Xe} = k_m (c_f - HRT \varepsilon^{-1} c_{s,surf.})$$

c : Species concentration (#/m³)
 λ : Species decay coefficient (1/s)
 l/g : Liquid/solid phase index
 D : Effective diffusivity (m²/s)
 ε : Porosity
 k_m : Mass transfer coefficient (m/s)



Species convection and diffusion in porous structures

Species reactivity feedback

$$\rho_{species} = \sum_n^N \alpha_n c_{phase}(t) V_{phase}$$

ρ : Reactivity ($\Delta k/k$)
 α : Species reactivity coefficient ($\Delta k/k$ per #)
 c : Species concentration (#/m³)
 V : Volume of phase (m³)