



Molten Salt Reactor P R O G R A M

# Salt and Materials Interaction

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Annual MSR Campaign Review Meeting 2-4 May 2023

# Acknowledgments

• Funding: DOE Office of Nuclear Energy, Molten Salt Reactor Campaign

#### ORNL team

- Dino Sulejmanovic: salt purification, handling and characterization
- Rishi Pillai: modelling
- Evangelia Kiosidou: electrochemistry (new)
- Adam Willoughby: thermal convection loops
- Yi-Feng Su and Michael Lance: characterization
- Jim Keiser, David Holcomb, Lou Qualls: consulting

• Kairos Power: salt (A. Kruizenga) and feedback (G. Young)



#### What are we afraid of?

- Inconsequential: Cr surface depletion
- Mass transfer
  - Block flow in channel!



Hastelloy N, NaBF<sub>4</sub>-NaF-KBF<sub>4</sub> 8760 h, TCL 605°-460°C - J. Koger, Corrosion, 1974



#### How do we study it?

- Flowing salt experiments
  - Forced convection loop
  - Thermal convection loop



#### How do we understand it?

- Dissolution experiments
  - Compare Cr and Fe in isothermal salt
  - Experiments in FLiNaK and FLiBe in progress
    - 550°-850°C





#### **ORNL FLiNaK pumped loop: prototypic conditions** But we first learn about corrosion on inexpensive TCLs



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# FLiNaK salt leak on 316H TCL





### Salt and Materials Interactions: R&D Goals

#### • FY22-23 goals

- Cr and Fe dissolution experiments in FLiNaK and FLiBe
  - FY22: Three temperatures: 550°, 650°, 750°C + three times (500-2000 h)
  - FY23: One temperature: 850°C + three times (100-2000 h)
- Continue to develop lifetime model (Pillai et al., JNM 2021, JOM 2023)

#### • Future topics

- FLiBe/316H interaction: higher temperatures/accident scenario TCLs
  - Feedback from MSR developer
- Compatibility effect of impurities/additives (salt purity standards)
- Further development of corrosion sensors/electrochemistry aspects
- Similar studies for CI salts

#### FY25 goal

- De-risk the transition from 316H to higher performance alloy 709
  - Focus on higher temperature operation and lifetime modeling





Unexpected temperature effect:

### Salt and Materials Interactions: FY22 overview

# • FY22 Carryover M3RD-23OR0603031: Measure Cr/Fe dissolution in FLiNaK and FLiBe

- Three temperatures (550°, 650°, 750°C) and three times (500-2000 h)
- Completed Cr in FLiNaK
- Repeating Fe in FLiNaK

M3RD-23OR0603032: Measure Cr/Fe dissolution at 850°C in two halide salts

- Three times (100-2000 h)
- More complete data set needed for modeling





## **Both Cr and Fe are dissolving**



FLiBe: low initial impurities No Be: Cr and Fe increase ≥90 ppm, Ni increase With Be: Cr and Mn increase (~45% less mass loss)



Temperature (°C)

## ICP-OES of FLiNaK: Increased Fe after 1,000h TCL



Evidence of Fe deposition in CL





#### Model can predict Cr depletion and depth of CI salt attack across different alloy chemistries at different isothermal temperatures: Need dissolution rates for model



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# Capsule testing to identify dissolution rates





100-2000 h in box furnace Flip at the end for removal 316L capsule (2<sup>nd</sup> containment)

graphite spacer

welded lid: no impurity ingress

Mo inner capsule

Argon (TIG weld in glovebox) vacuum (EB weld)

~30 g purified FLiNaK/FLiBe salt

Cr or Fe: 12 x 20 x 1.5mm

Mo wire





### Dissolution mass losses: 500-2000 h at 550°-750°C

#### • Mo capsules

- standard ORNL procedure
- Purified FLiNaK salt (+400ppm Zr)
- Little change with longer time except for Fe specimens at 750°C





## Uh oh: low Fe in salt after 750°C tests Cr somewhat consistent



- Mo-Fe interaction
  - Capsule effect!
- Need to repeat test with Fe capsule
  - First tests no Fe sample
  - Waiting for ICP-OES analysis of tests at 550°-850°C
  - Next tests will include Fe specimen

#### To validate model in flowing salt: Need to characterize FLiNaK/316H loop



Topmost section of hot leg (~647 °C) shows dissolution of Cr, Mn, Fe and Mo





# 316H tubing attack was observed to decrease from the top to the bottom of the TCL hot leg





#### Measured concentration profiles suggest depletion of all key elements

**Depth of attack** 





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#### Topmost section of cold leg (~604 °C) shows deposition of Fe-rich oxides





# Bottom section of cold leg (~542 °C) shows deposition of Ti-rich oxides (most likely from alloy 600 wire used to hold the specimens)



# <u>Hypothesis</u>: Corrosion of alloying constituents is primarily governed by their chemical activity (thermodynamics) and mobility (kinetics) in the alloys



• Calculation of phase equilibria

- Calculate diffusion in the alloy
  - Using measured Cr and Fe concentrations after exposure of pure Cr and Fe in purified FLiNaK
  - Use of independent thermodynamic-kinetic data -TCNI/MOBNI (Thermo-Calc)
  - Consideration of relevant elements & phases in commercial high temperature alloys and coating systems
  - Mesh adaption accounts for surface recession (predictions for metal loss)
  - Thermodynamic calculations on multiple cores

#### Cr loss from 316H is expected to slightly increase with temperature while Fe loss significantly drops at lower temperatures





#### Calculated time evolution of Fe and Cr surface activity shows Fe dissolution begins after Cr is saturated in the salt



- Saturation limit (~280 ppm) was measured in FLiNaK dissolution tests
- Much slower Fe dissolution rate was derived from dissolution tests



## Next: effect of temperature + testing in FLiBe



#### Initial 850°C results: less Cr loss

FLiBe salt arrived from Kairos Capsules being assembled





## Path forward: modeling dissolution in purified, flowing salt

- Model used Cr data in Cl salt
  - Pillai et al., JNM 2021, Ni-Cr alloys
  - Pillai et al., JOM 2023, Fe-Cr alloys
- Collecting dissolution data in FLiNaK and FLiBe
- Current task to model dissolution and mass transfer in flowing salt



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## Gordon Conference on High Temperature Corrosion

- July 16-21, 2023
- Colby Sawyer College
  - New London, NH
- You're all invited to attend
- For students and early career:
  - Gordon Research Seminar 7/15-16





# Thank you

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