

# Experiments and computations to address the safety case of heat pipe failures in Special Purpose Reactors

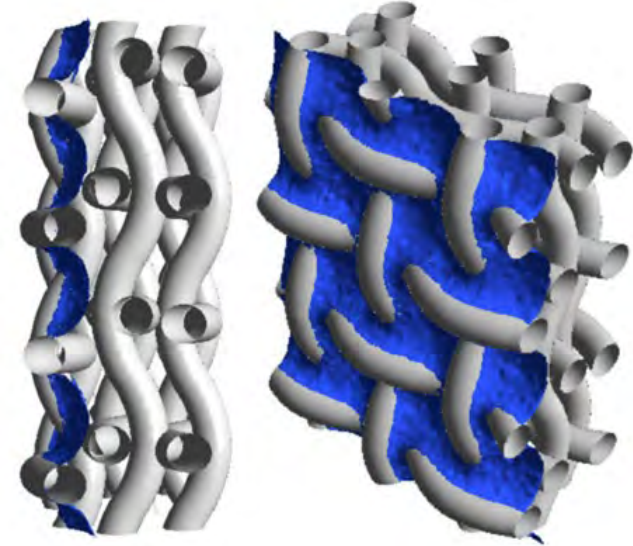
**(NEUP Project 19-17416)**

Date: March 6<sup>th</sup>, 2024

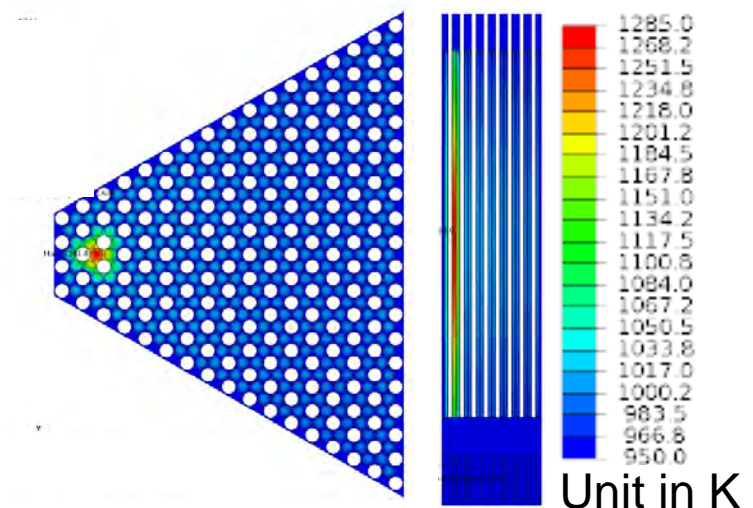
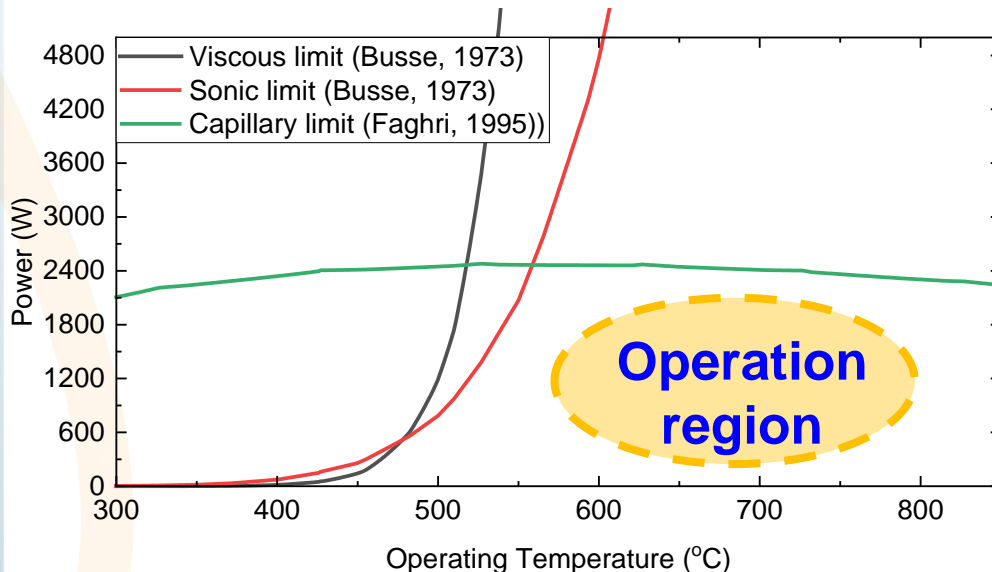
Authors: Victor Petrov, Annalisa Manera, Pei-Hsun Huang, Taehwan Ahn

# Project overview

- Development of special purpose reactor
  - Heat pipe operation principle
  - Heat pipe modeling
- Knowledge gaps
  - The two-phase flow phenomena in heat pipes
  - Effect of parameters on heat pipe performance
  - Integral study on microreactors



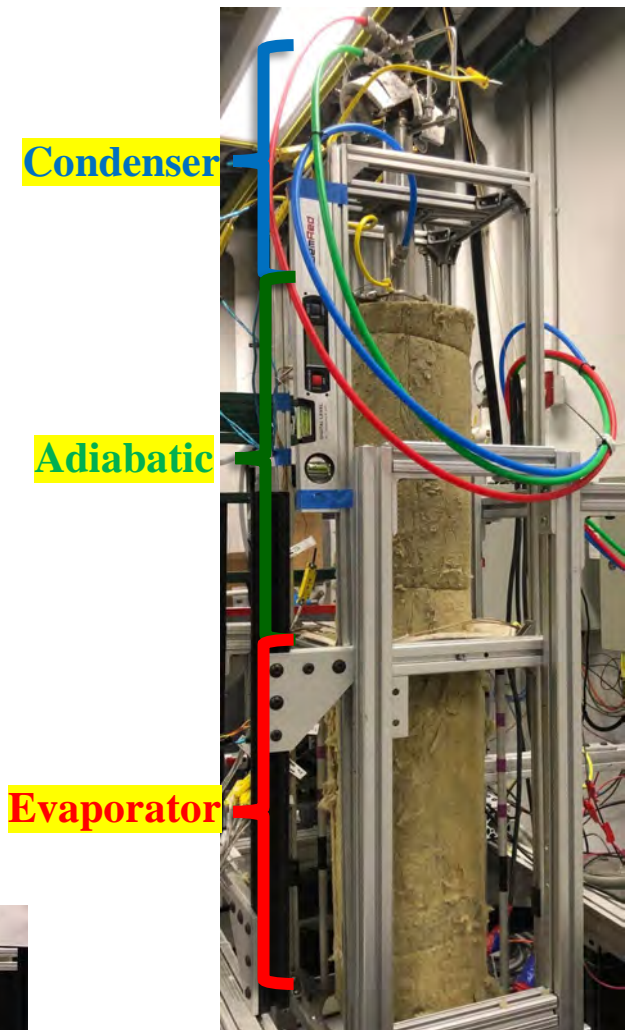
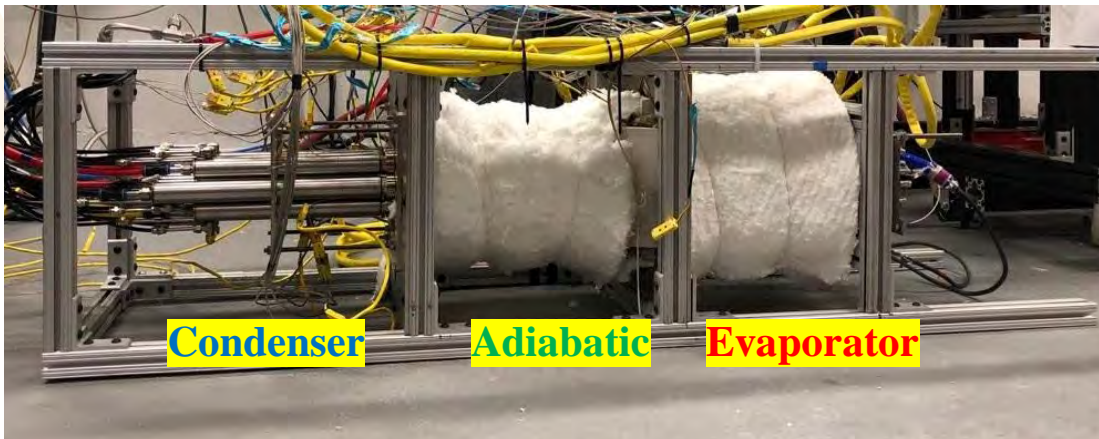
(Dutra et al., 2022)



(McClure et al., 2015)

# Project goal

- Separate effect of single sodium heat pipe
  - Parameter investigation
    - Heating condition - Input power
    - Cooling condition - Heat transfer coefficient of heat exchange
    - Inclination angles
    - Sodium content in heat pipe
  - X-ray radiography measurement
- Integral effect of heat pipes bundle
  - Startup process
  - Normal operation
  - Non-uniform boundary conditions
  - Abnormal scenarios (1 or 2 heat pipe failure)



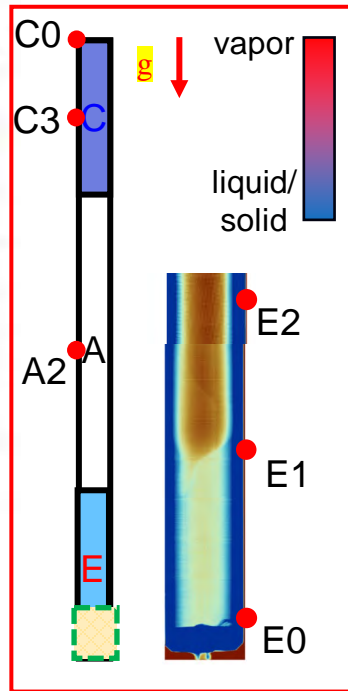
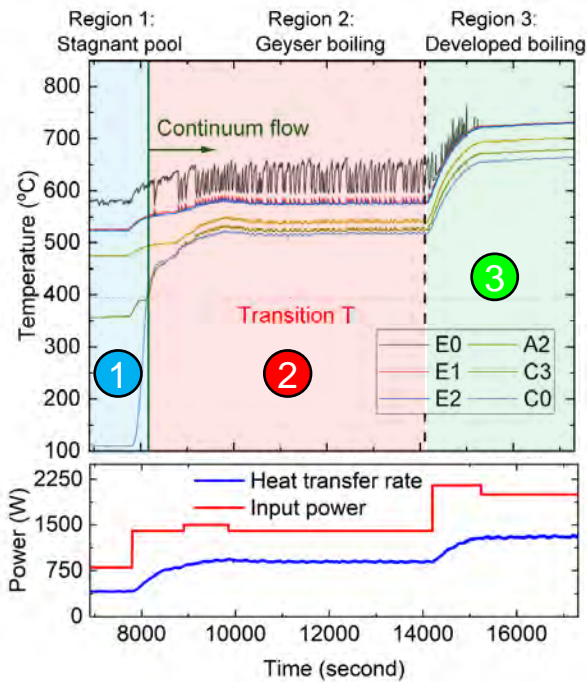
**Michigan Sodium Heat pipe test facility, MISOH1**

Separate effect of single sodium heat pipe:

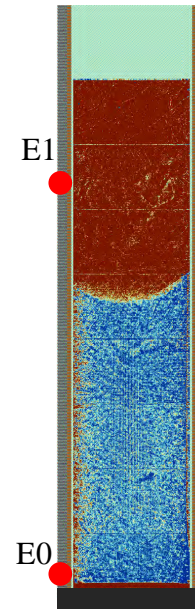
# Michigan Sodium Heat pipe test facility (MISOH1)

# Separate effect of single sodium heat pipe – MISOH1 test facility

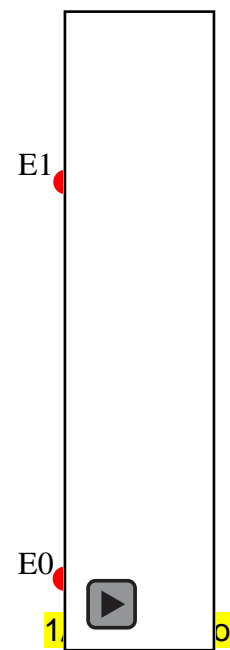
- Sodium flow characteristics (temperature and x-ray image/video)



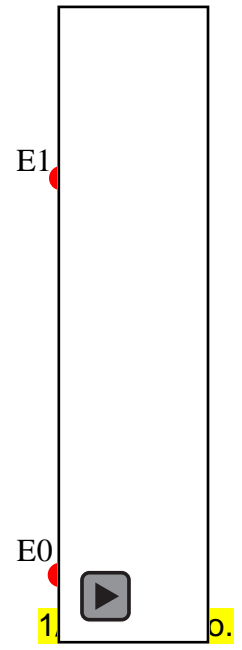
Region 1: Stagnant pool



Region 2: Geyser boiling



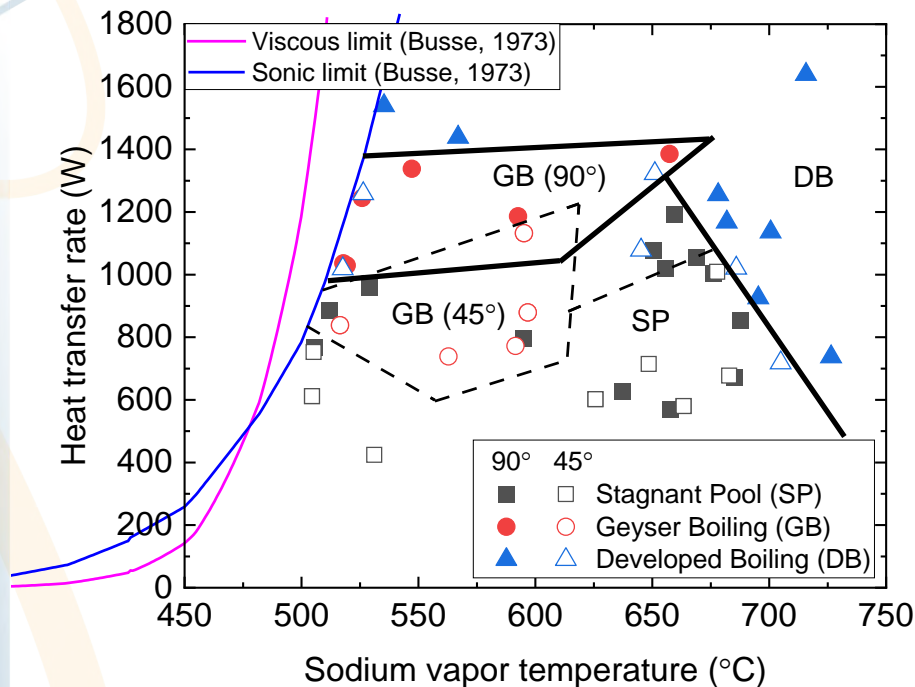
Region 3: Developed boiling



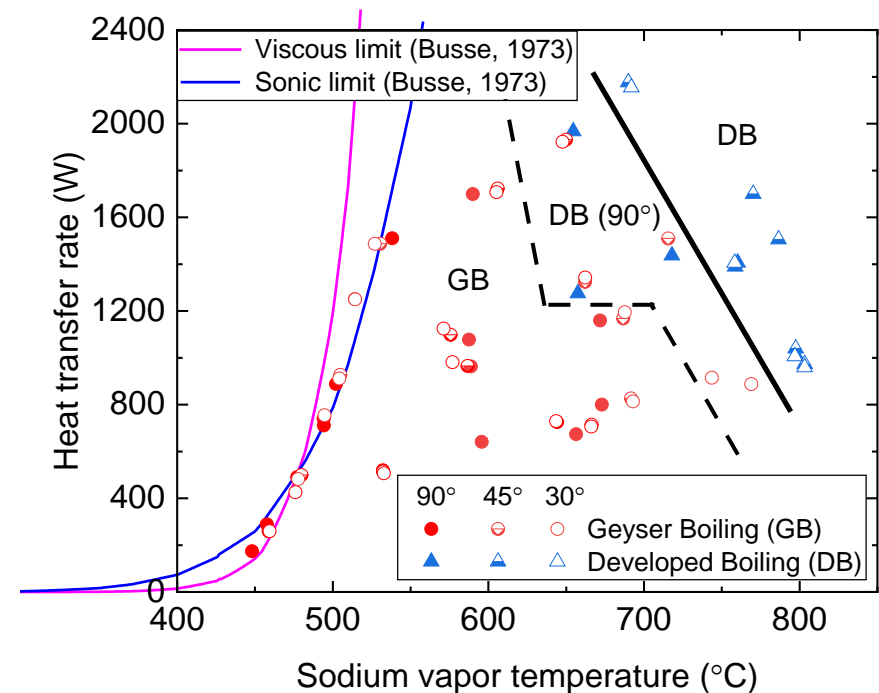
# Results: 2. Flow characteristics

## •Boiling flow regime map

–The initiation of boiling phenomena is closely related to the sodium filling ratio in the heat pipe and the orientation of heat pipe



**Filling ratio = 102%**



**Filling ratio = 172%**

Integral study on microreactors

**Michigan Sodium Heat pipe bundle test  
facility (MISOH2)**

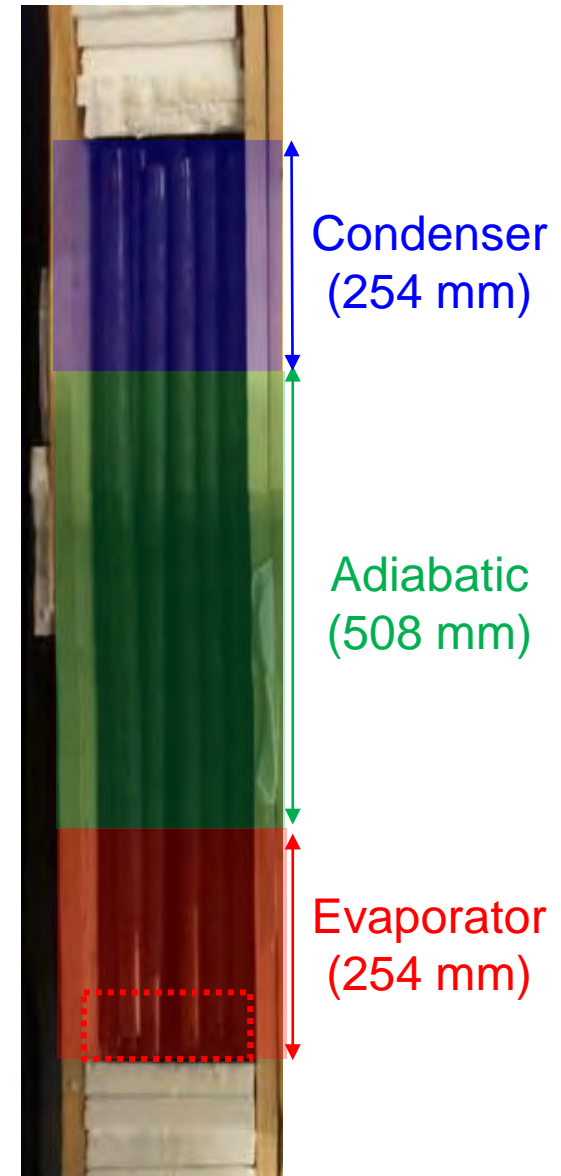
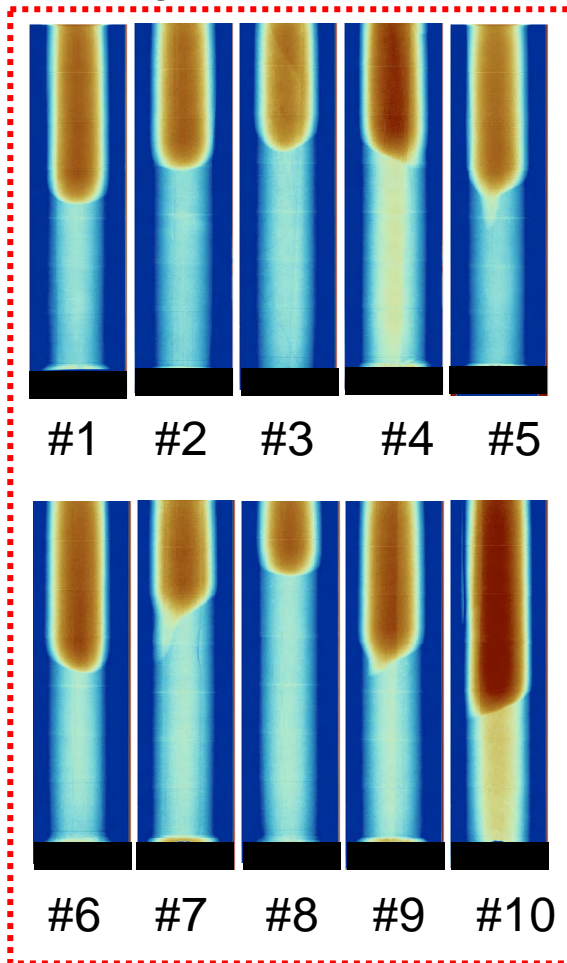
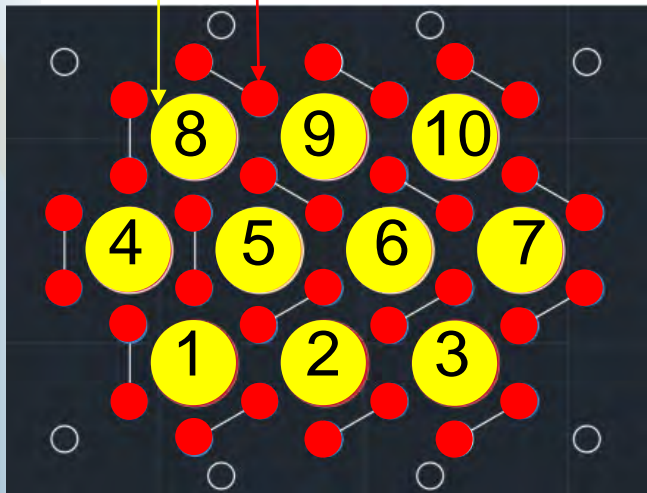
# MISOH2 heating elements and heat pipes layout

Specification of the MISOH2 facility design

- Ten heat pipes hexagonal array
- 32 holes allocated for heating elements
- Sodium contents in selected heat pipe
  - 27 - 35 grams (80 – 110% filling ratios)

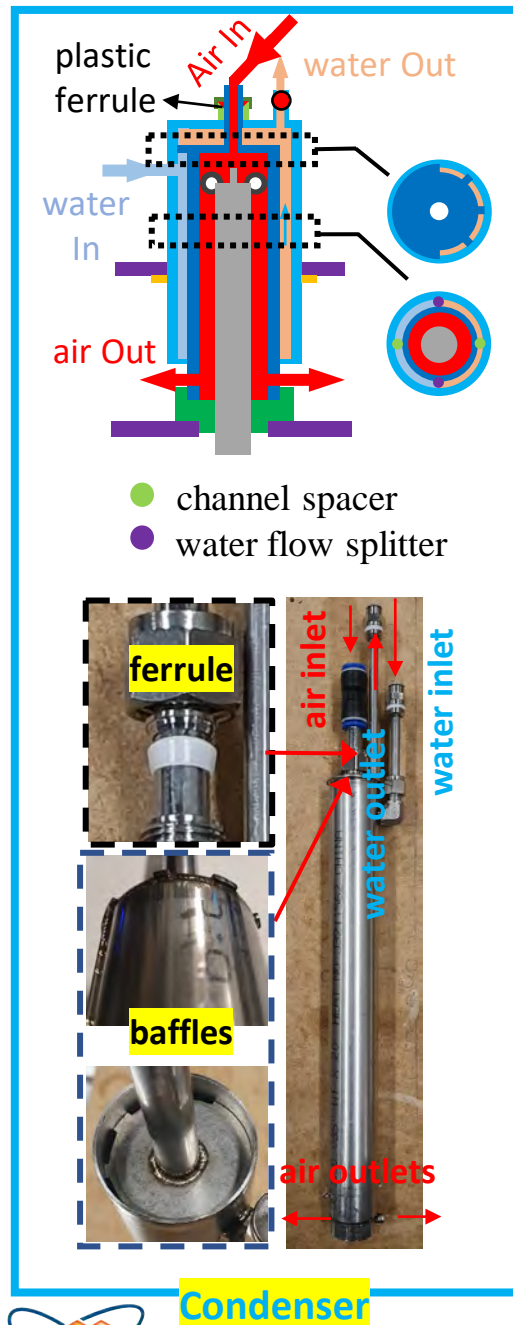
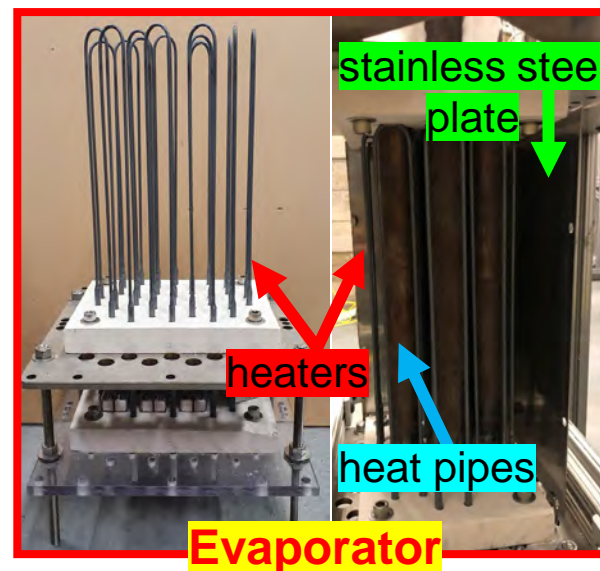
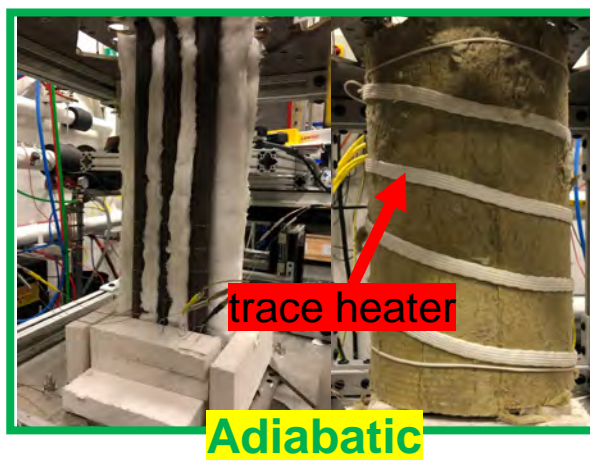
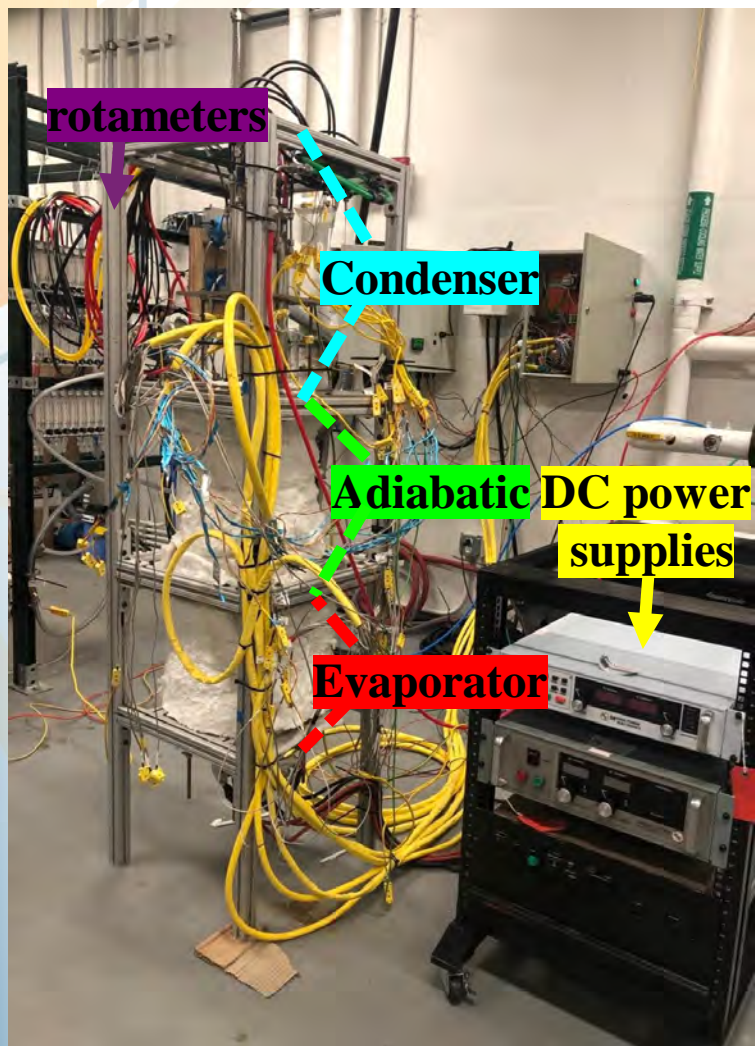
Heat pipe (22.1 mm ID)

Heating elements  
(3 mm OD)



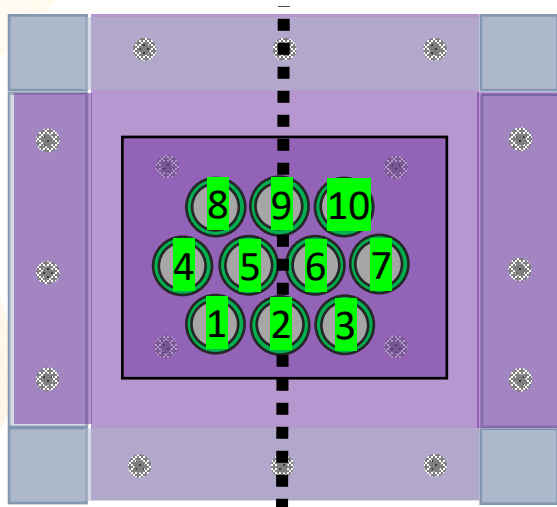


# Experimental apparatus

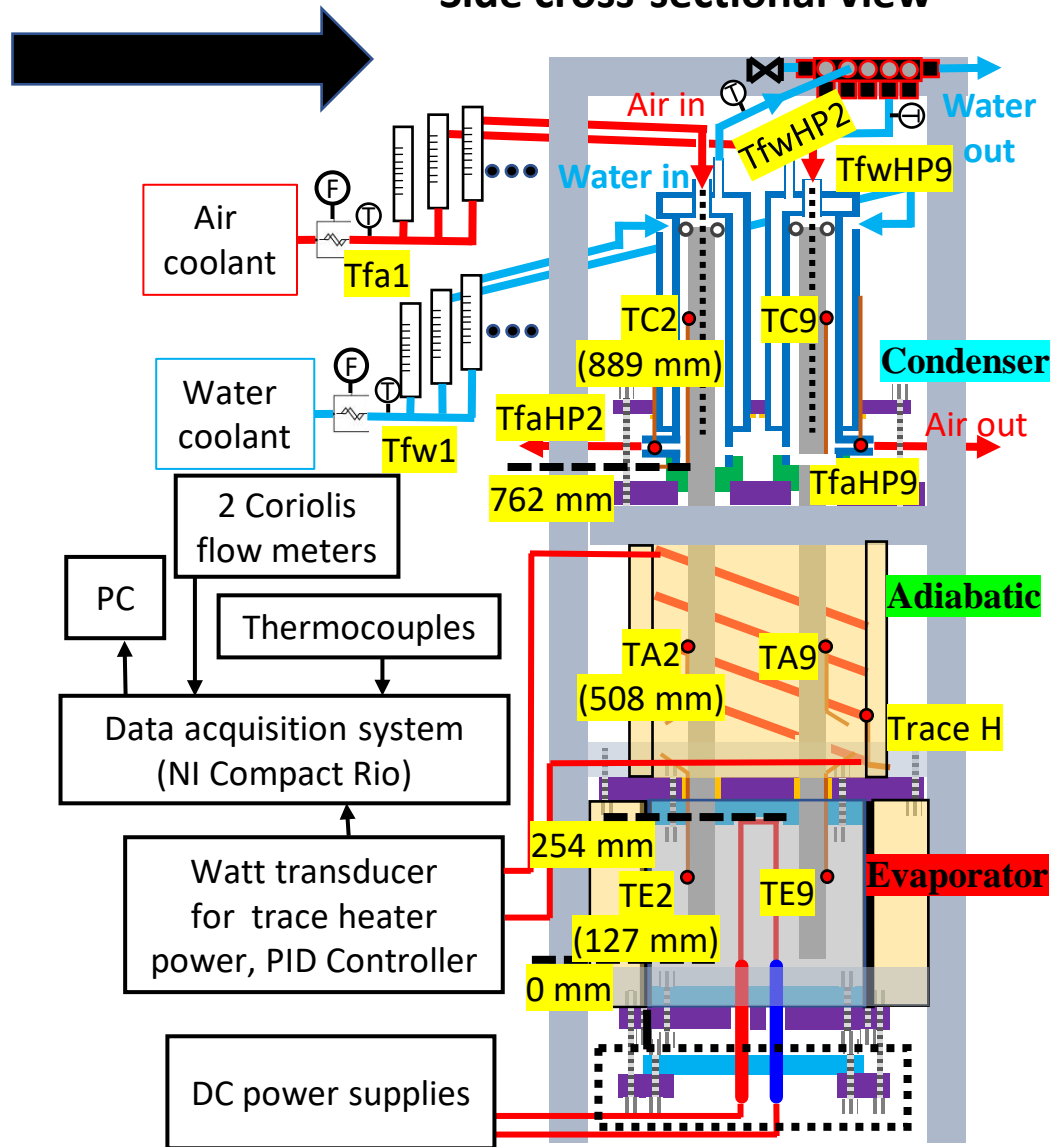


# Experimental apparatus

Top cross-sectional view



Side cross-sectional view

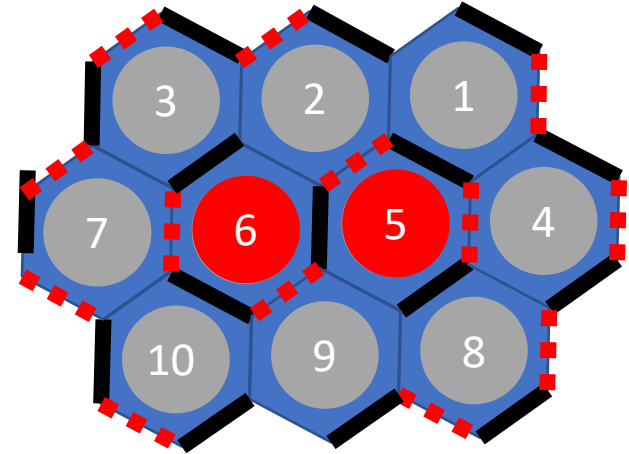


- Heat pipe
- 1.5"x1.5" Al extrusion
- 1" machined collar
- Calcium Silicate insulation
- Spacer plates
- Insulator

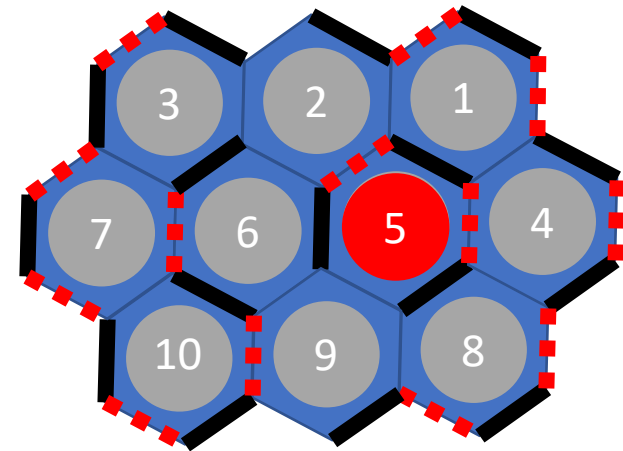
# Case Study

- Normal operation
  - Change of input power
  - Change of cooling intensity
  - Change of inclination angle
- Non-uniform boundary conditions
  - Change of cooling intensity on individual heat pipe
  - Change of heat flux with different grouping of heating elements
- Abnormal operation
  - Replacing one heat pipe (HP05) with dummy stainless-steel tube
  - Replacing two heat pipes (HP05 and HP06) with dummy stainless-steel tubes

— Heating element ■■■ Busbar connector



Normal operation (double heat pipe failure)



Normal operation with non-uniform heat flux (single heat pipe failure)

# Data reduction

- Heat transfer rate of heat pipe:

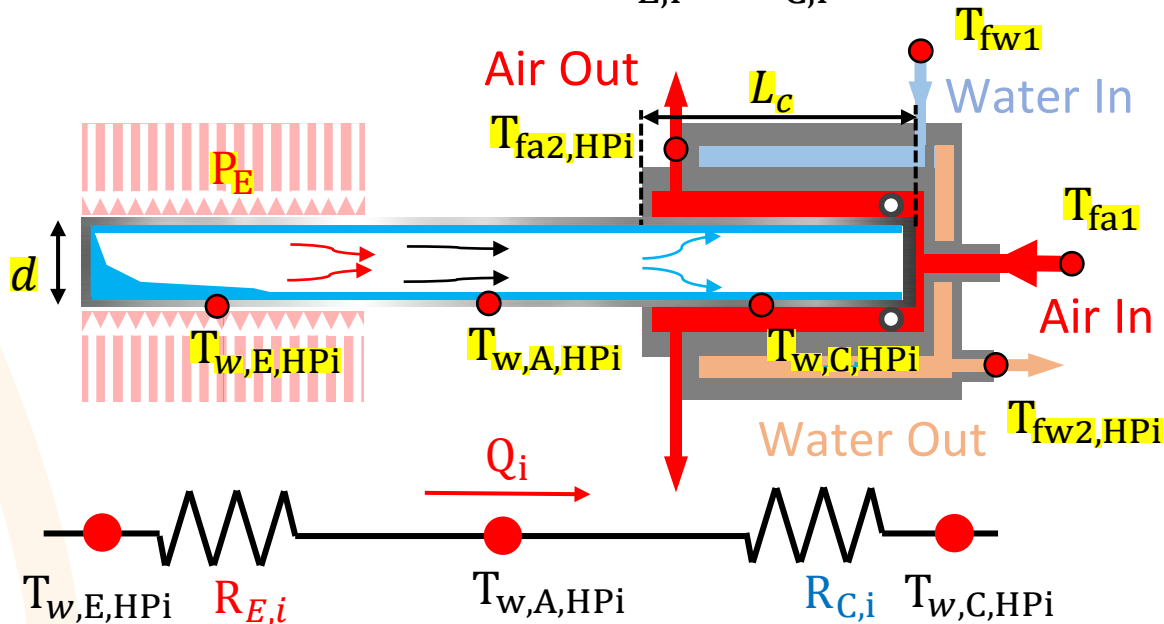
$$Q_{HPi} = c_{p,w} \dot{m}_{w,HPi} (T_{fw2,HPi} - T_{fw1}) + c_{p,a} \dot{m}_{a,HPi} (T_{fa2,HPi} - T_{fa1})$$

- Heat transfer coefficient of heat exchanger:

$$h_{hx,HPi} = Q_{m,HPi} / [\pi d L_c (T_{w,C,avg,HPi} - T_{fm,avg,HPi})]$$

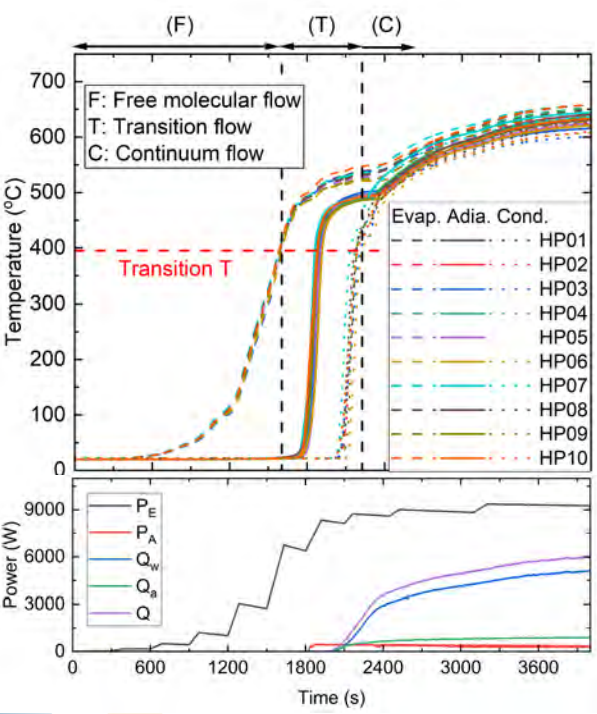
- Effective thermal resistance:

$$R = R_{E,i} + R_{C,i}$$

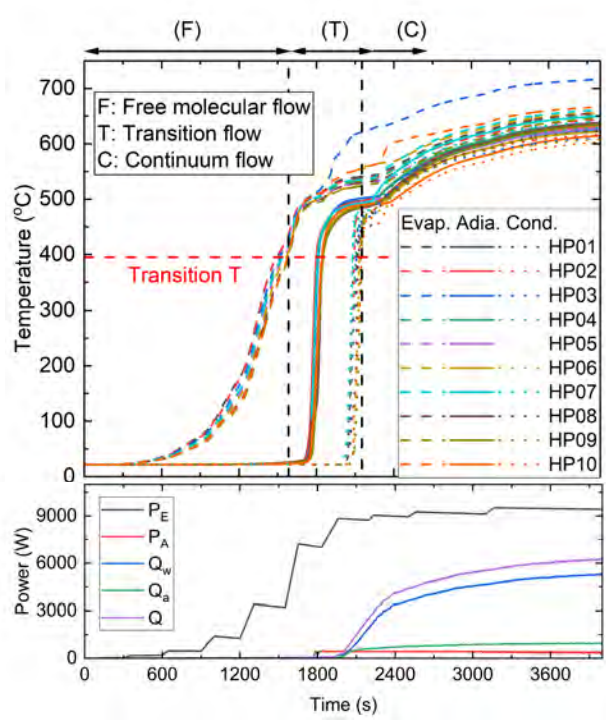


# Results 1: Uniform boundary conditions – startup process

- Successful startup of heat pipes bundle at 9 kW of heating power (6 kW heat transfer rate).
- Time characteristics is similar between the two orientations.

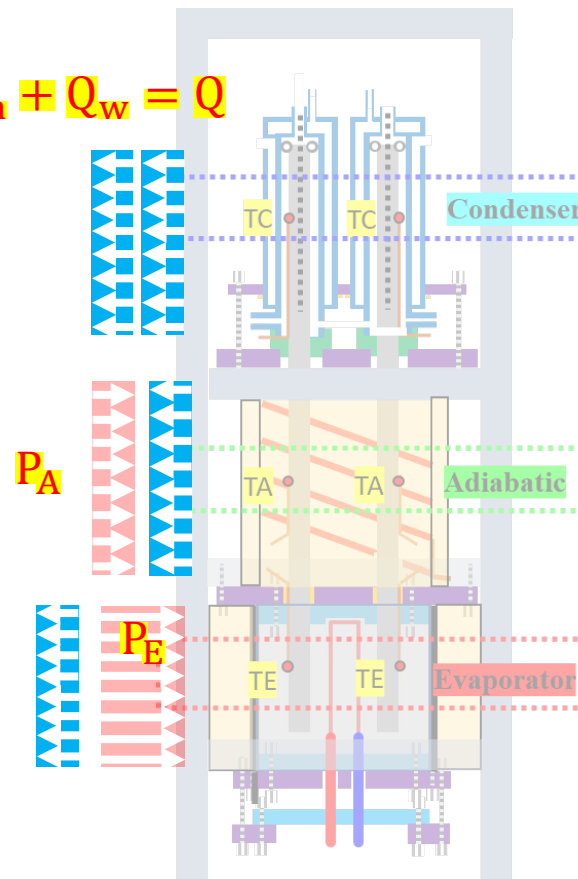


Vertical orientation



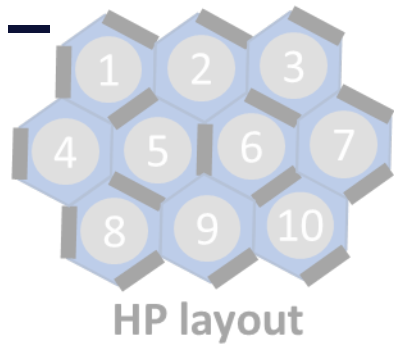
Horizontal orientation

$$Q_a + Q_w = Q$$



# Result 1: Uniform boundary conditions – steady-state operation

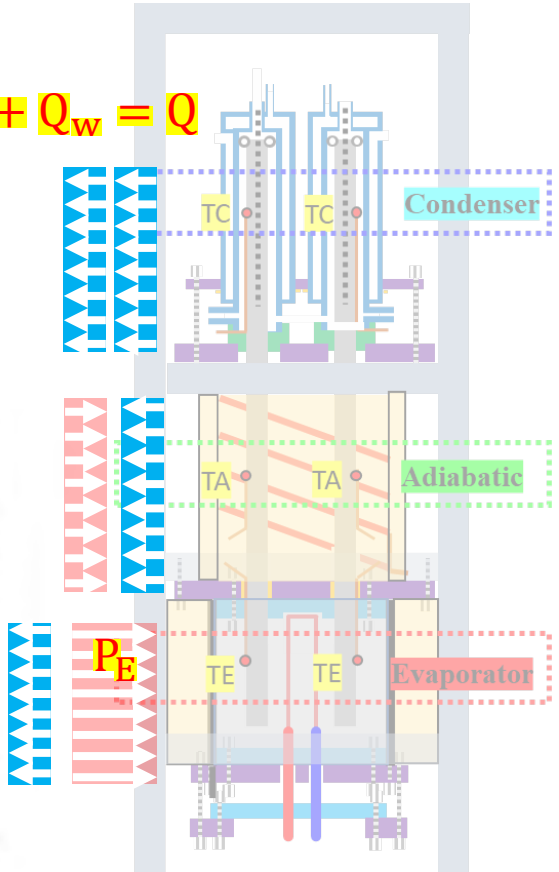
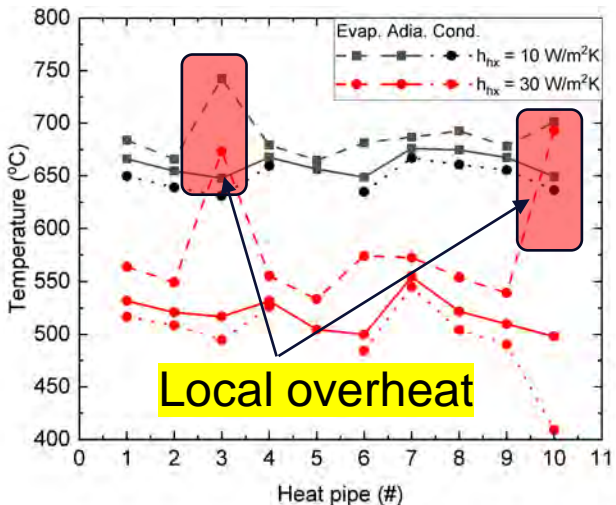
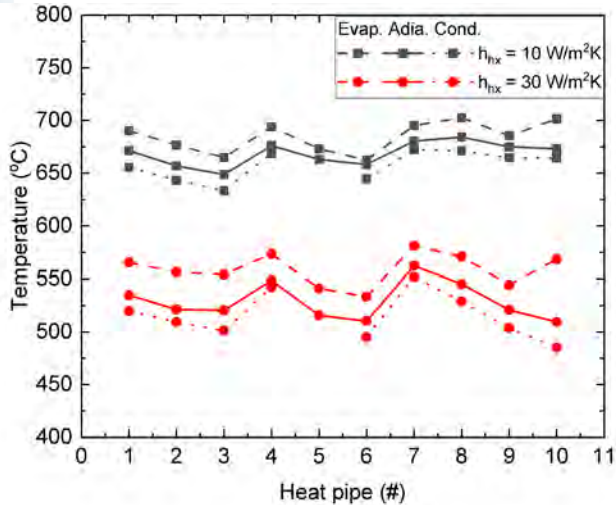
- The temperature is not uniform even with uniform boundary conditions, especially under horizontal orientation
- These cases serve as references for the scenarios of abnormal operation



$$Q_a + Q_w = Q$$

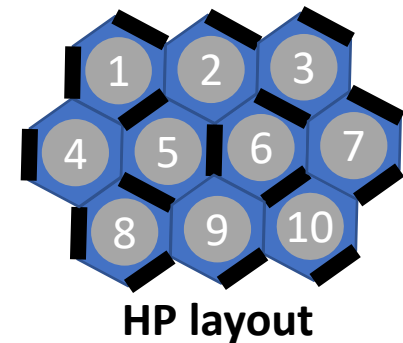
- Vertical orientation (90°)
- P = 10 kW
- Q = 6.5 kW

- Horizontal orientation (0°)
- P = 10 kW
- Q = 6.5 kW

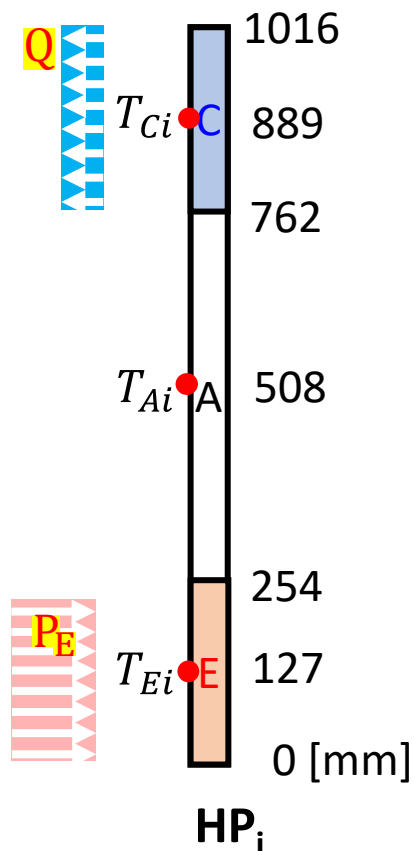
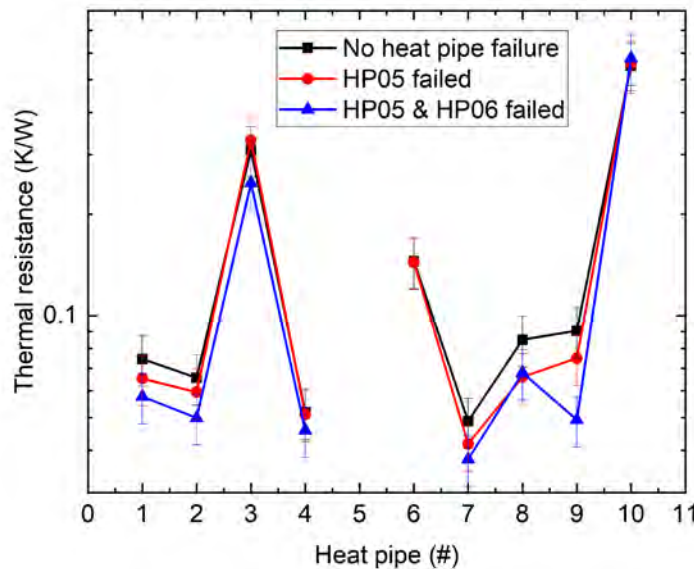
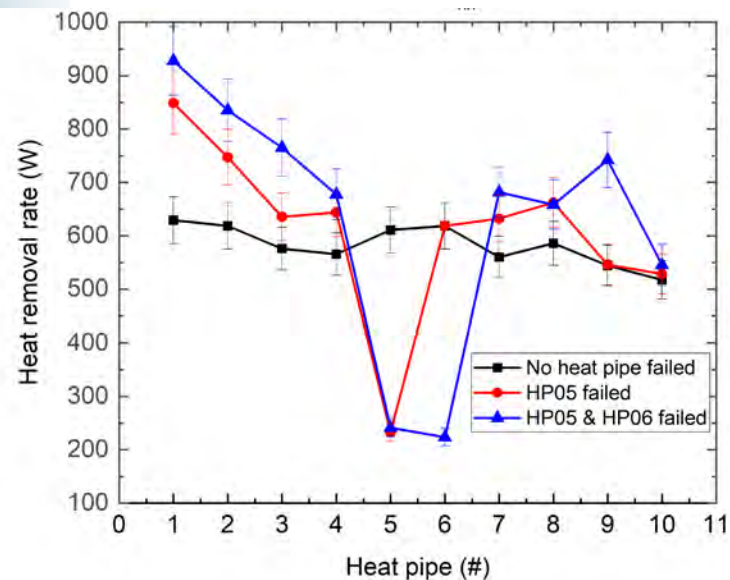


# Result 3: Heat pipe failure events – steady-state operation

- Error bars applied based on error propagation
- Neighboring heat pipes compensate for the heat transfer under abnormal scenarios
- The performance of neighboring heat pipes was maintained without increasing effective thermal resistance

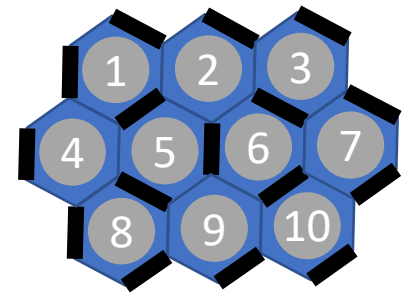
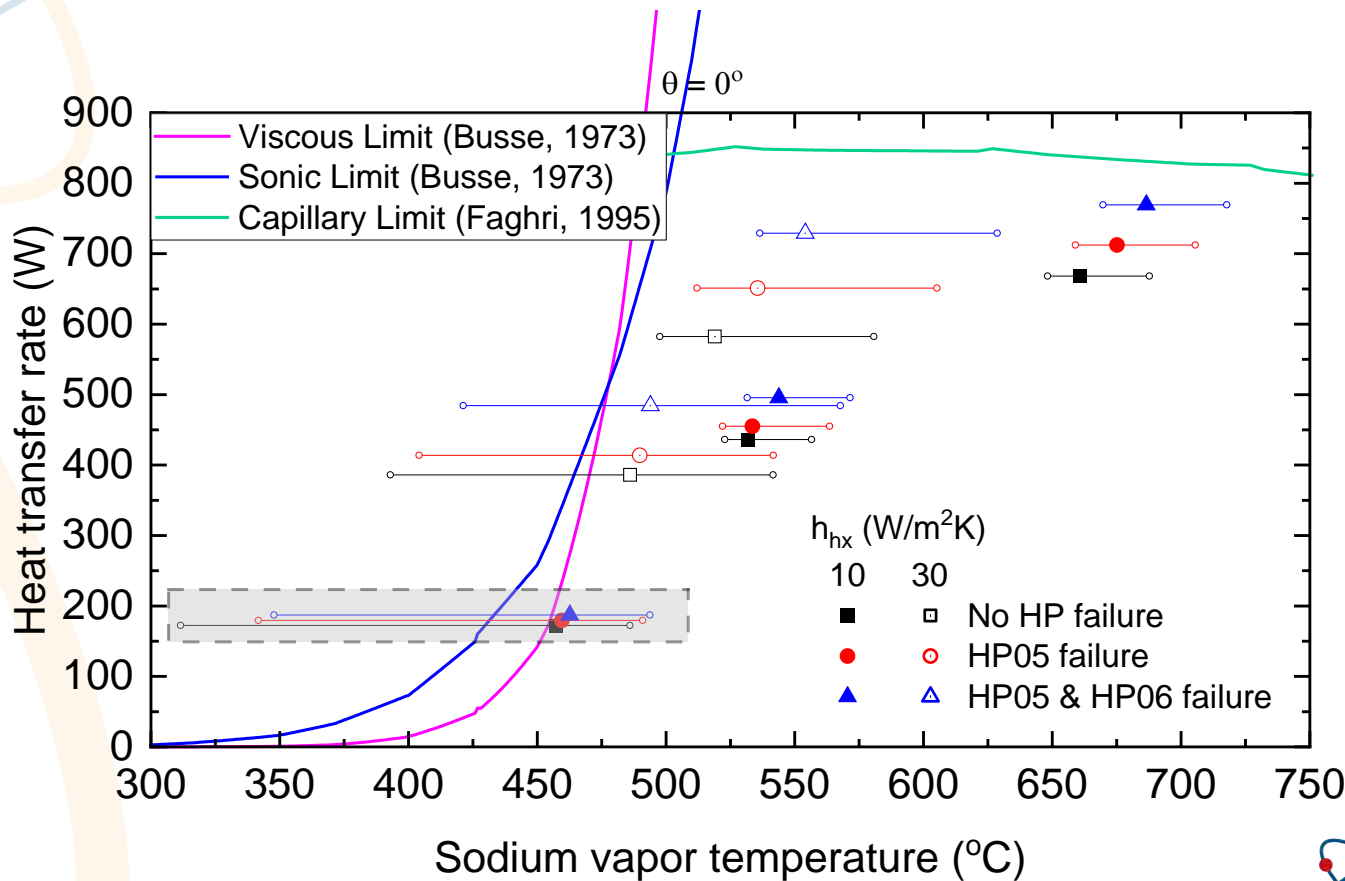


Test condition:  $\theta = 0^\circ$ ,  $P_E = 10 \text{ kW}$  ( $Q = 6.5 \text{ kW}$ ),  $h_{hx,HPi} = 30 \text{ W/m}^2\text{K}$

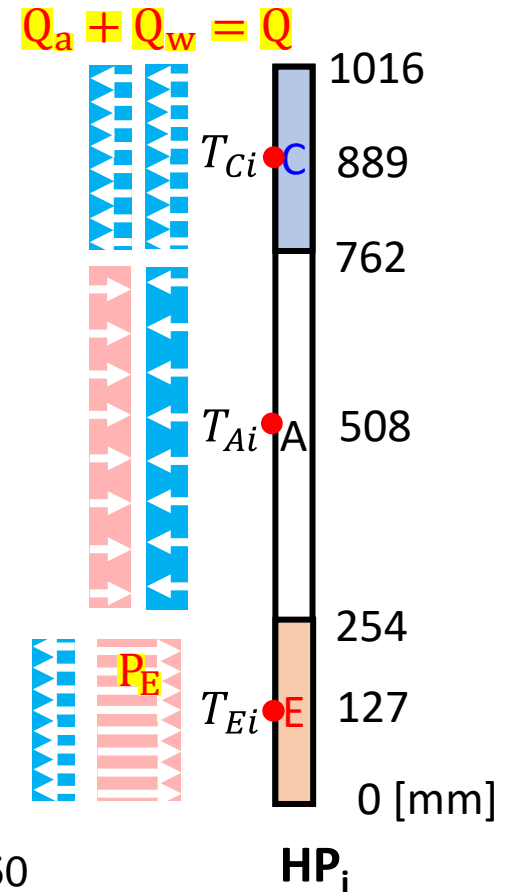


# Result 4: Heat pipe operation map

- End-to-end temperature decreases with heat pipe failure events when operating near viscous limit
- Average heat pipe operation (excluding failed) sees an increase in vapor temperature and heat transfer rate with heat pipe failure events



HP layout





# Conclusion

Separate effect of single heat pipe

- Boiling phenomenon
- Heat pipe operation map

Integral effect of heat pipes bundle

- The startup time characteristics is similar regardless of inclination angle and the failure of heat pipe(s)
- Vertical orientation yields more uniform temperature distribution than horizontal orientation
- Show effect of non-uniform heating and cooling conditions on neighboring heat pipes
- Show effect of single heat pipe failure and double heat pipe failure
  - Neighboring heat pipes can compensate for the heat of transfer of failed heat pipes
  - The operation condition of neighboring heat pipes shifts while maintaining ideal performance



# Thank you For your attention Questions

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**MRP** Microreactor  
Program