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# Molten Salt Reactor Chlorine Radioisotopes Separation by Electrophoresis

Shirmir Branch, Marsobyn Salalila, Jason Serkowski, Cornelius Ivory (WSU) , Danny Bottenus  
Pacific Northwest National Laboratory and Washington State University



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# Overview

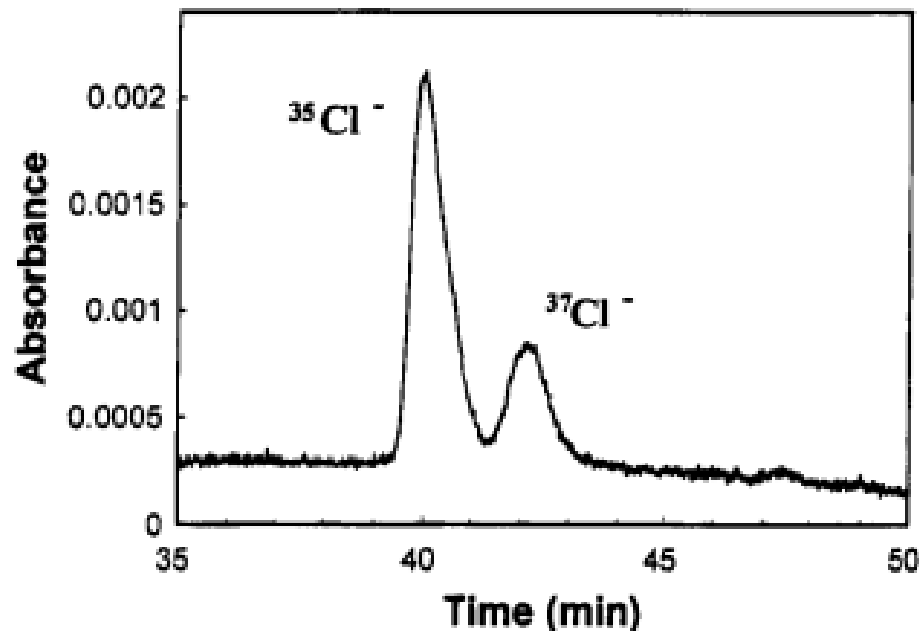
- **Introduction**
  - Electrophoresis fundamentals
- **Review of bench-scale electrophoretic equipment**
  - Cl isotopic analysis by QQQ-ICPMS
  - Comparison of experimental with simulation results
- **Experimental results**
- **Recycle continuous flow electrophoresis design**
- **Conclusions**

# Introduction

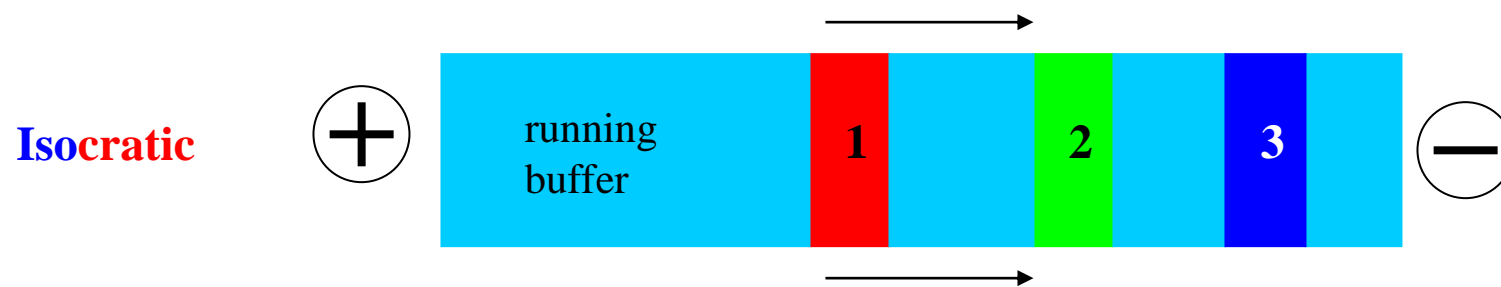
- **Design for molten salt reactors**
  - Rely on fluoride or chloride-based salts to act as coolants or fuel carriers
  - Chloride salts have attractive features
    - Actinide trichlorides forms lower melting point solutions and have higher solubility for actinides so they can contain significant amounts of transuranic elements
    - $^{35}\text{Cl}$  has a strong (n, proton) threshold reaction that will poison the reactor and gives rise to  $^{36}\text{Cl}$  as an activation product, which is a long-lived, energetic beta source that complicates waste disposal
      - Cl isotope ratio =  $^{35}\text{Cl}$  (75.77%),  $^{37}\text{Cl}$  (24.23%)
  - Currently no domestic capability to enrich  $^{37}\text{Cl}$  from the more abundant  $^{35}\text{Cl}$

# Electrophoresis

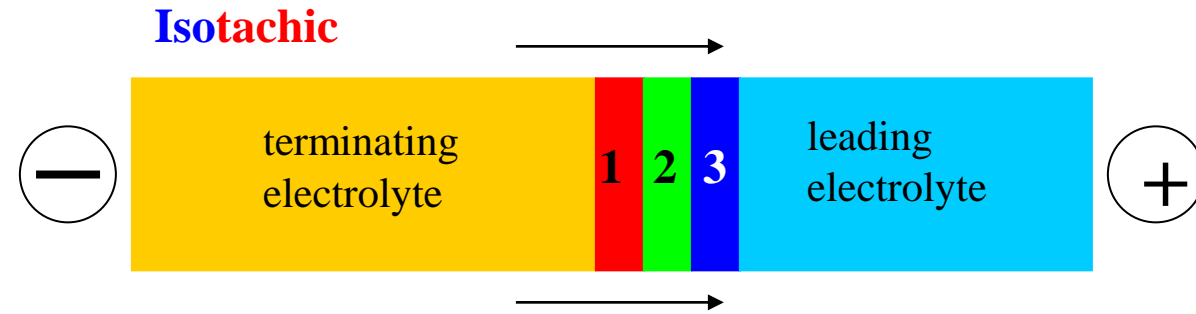
- Enrichment and separation of  $^{37}\text{Cl}$  from  $^{35}\text{Cl}$  at nanogram scales by capillary electrophoresis (CE) has been demonstrated in the technical literature
- Electrophoretic mobility difference is 0.29%
  - $^{35}\text{Cl}$  mobility =  $79.18 \cdot 10^{-9} \text{ m}^2/(\text{V}\cdot\text{s})$
  - $^{37}\text{Cl}$  mobility =  $78.95 \cdot 10^{-9} \text{ m}^2/(\text{V}\cdot\text{s})$
- Elemental chloride has been separated by isotachopheresis (ITP)
- Propose stationary ITP and Moving Bed Electrophoresis (MBE) for enrichment



## Capillary Zone Electrophoresis (CZE)



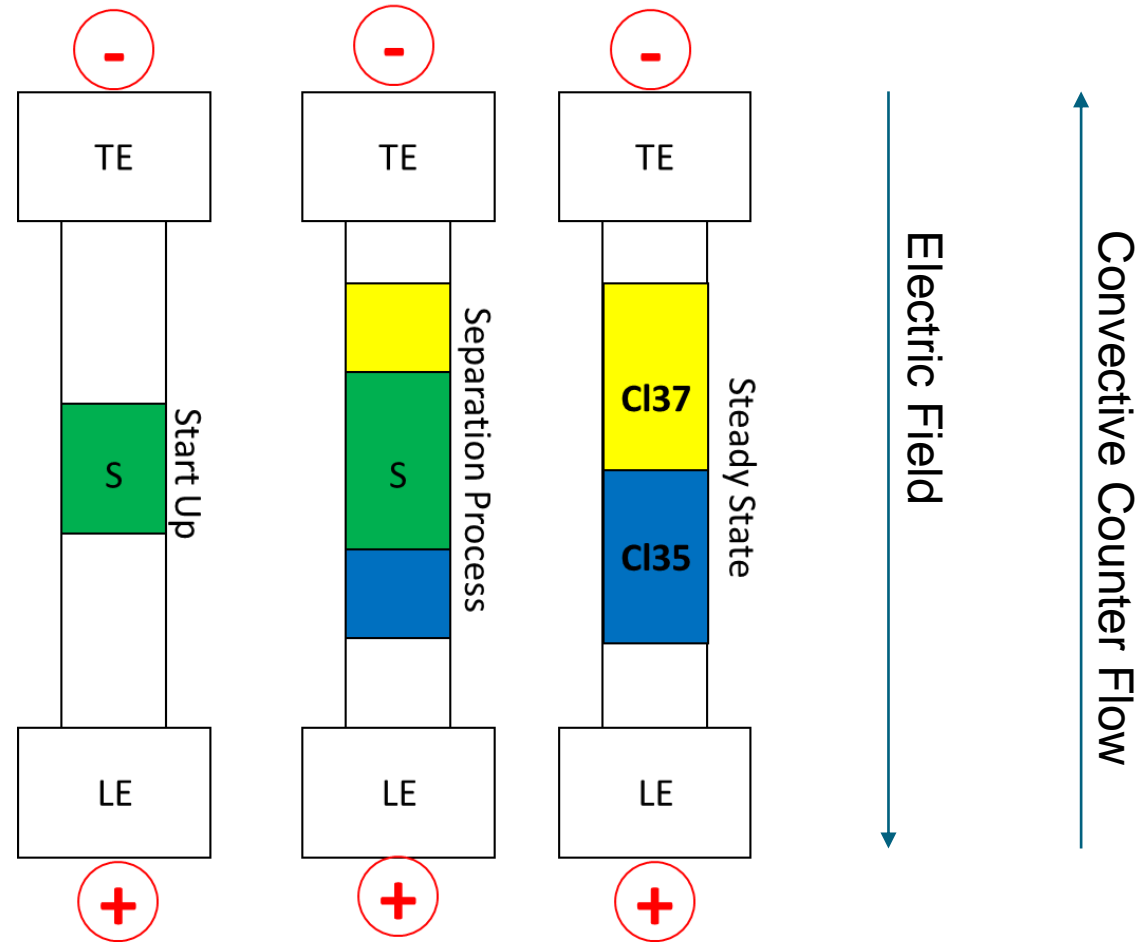
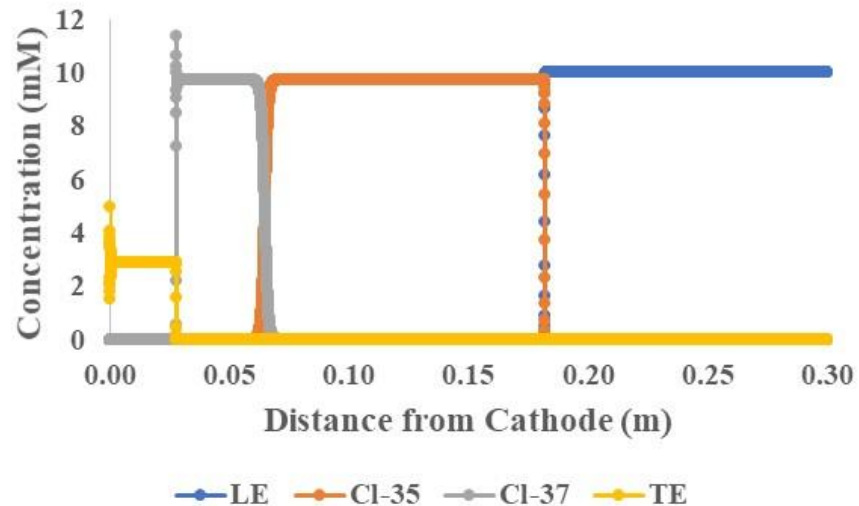
# Isotachopheresis



- Separation and pre-concentration of charged analytes in an electric field
- Sample (S) is introduced between a fast-leading electrolyte (LE) and a slow terminating electrolyte (TE)
- Apply electric field and ions will migrate according to their  $\mu_i$ 
  - $\mu_{LE} > \mu_S > \mu_{TE}$
- Advantages
  - Concentration by several orders of magnitude
  - Simple, fast, and compatible with other analytical techniques
  - Simultaneous concentration/fractionation
  - Immune to racetrack dispersion
    - ITP self-sharpening effect
  - “Greener” technology
  - Chemical reagents needed are less hazardous than alternative approaches
  - Potential to out-perform liquid:liquid extraction approaches

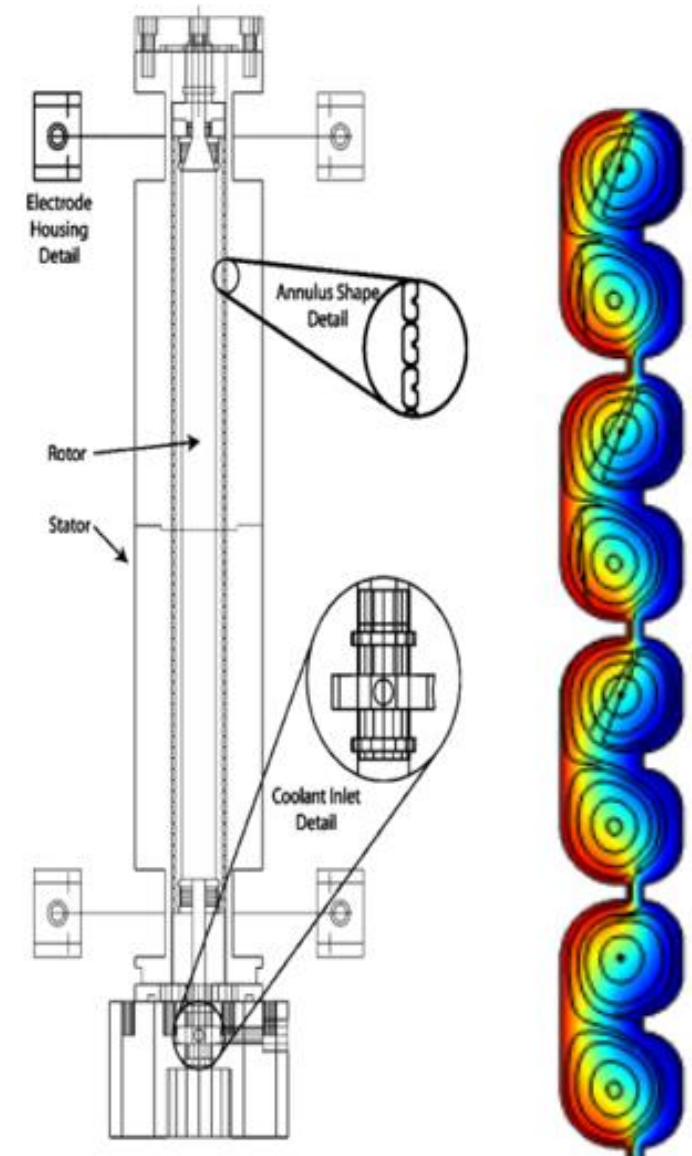
# Stationary Isotachopheresis

- Balance electric field with “upflow” counter flow
- Allows time for difficult separations
- May take up to days to get complete separation under ideal conditions
  - pH excursion issues, i.e. hydrogen build-up at cathode
- New capability to PNNL



# State of the Art Electrophoresis System

- Separation medium is in the annulus
- Complimentary tines and spinning rotor → No electroosmotic Flow
- Cooling oil is recirculated through the hollowed-out rotor that effectively remove Joule Heat
- Equipment can be modified to run in continuous operation
- Sample ports along the length of the chamber allow for easy sample collection
- Efficient removal of electrolysis products



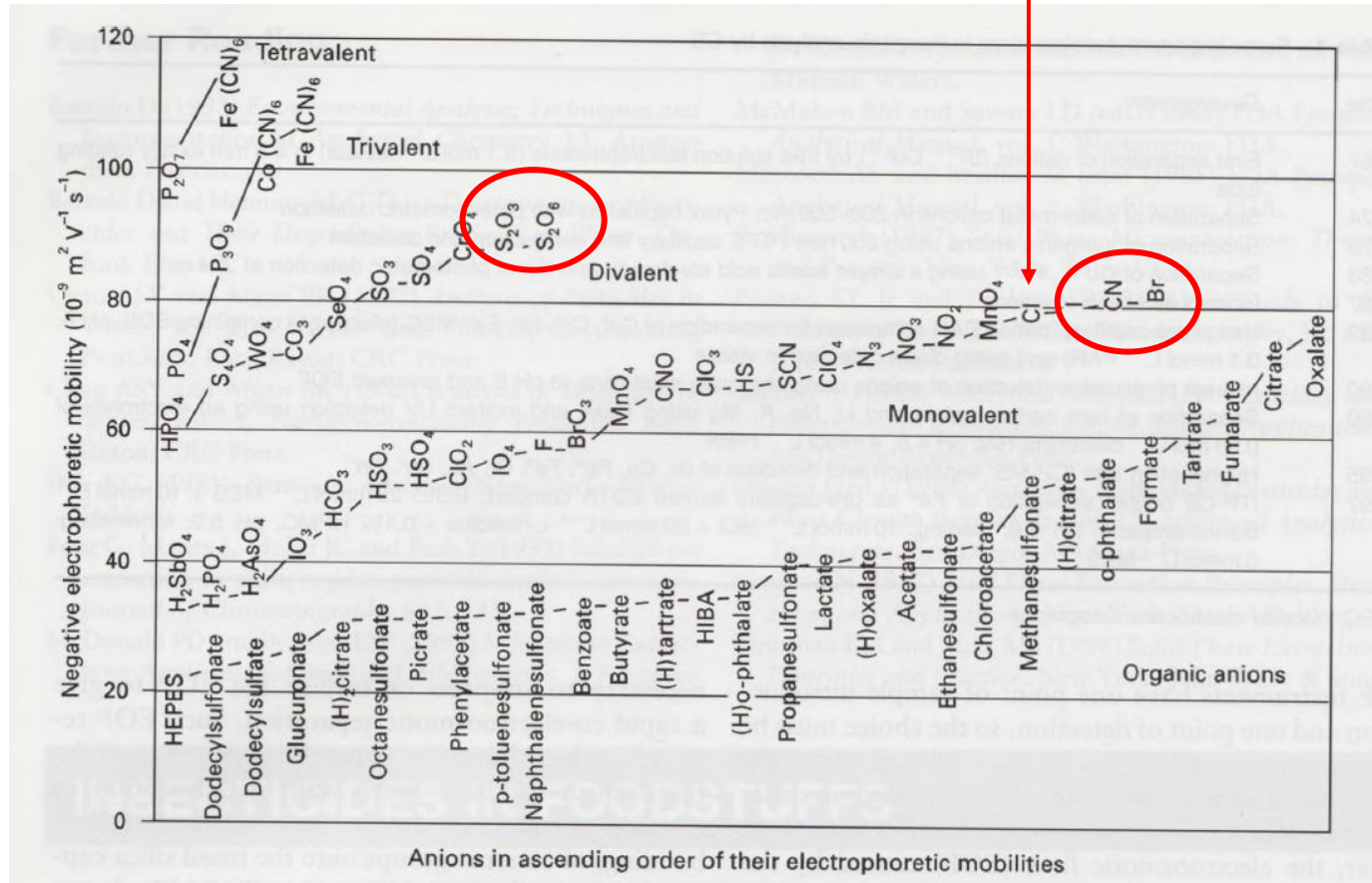
# Challenges

- Initial literature review found thiosulfate and dithionate as strong candidate for LE in ITP separations
- Neither ion was available and required a custom synthesis that made the cost and time to synthesis prohibitive
- Other options Br, I, and CN were safety concerns
- Resulted in a pivoting of strategy
  - Initial testing at PNNL utilized moving bed electrophoresis (MBE)
  - QQQ-ICPMS for analysis of separation efficiency

Operational system	Leading	Terminating
Solvent	Water	Water
Anion	Dithionate	Citrate
Concentration (mmol/l)	5	5
Counter ion	$\beta$ -Alanine	-
Co-counter ion	$1.8 \text{ mmol l}^{-1} \text{ Mg}^{2+}$	-
Additive	0.1% HMEC	-
pH	3.5	ca. 4

HMEC = hydroxymethylcellulose.

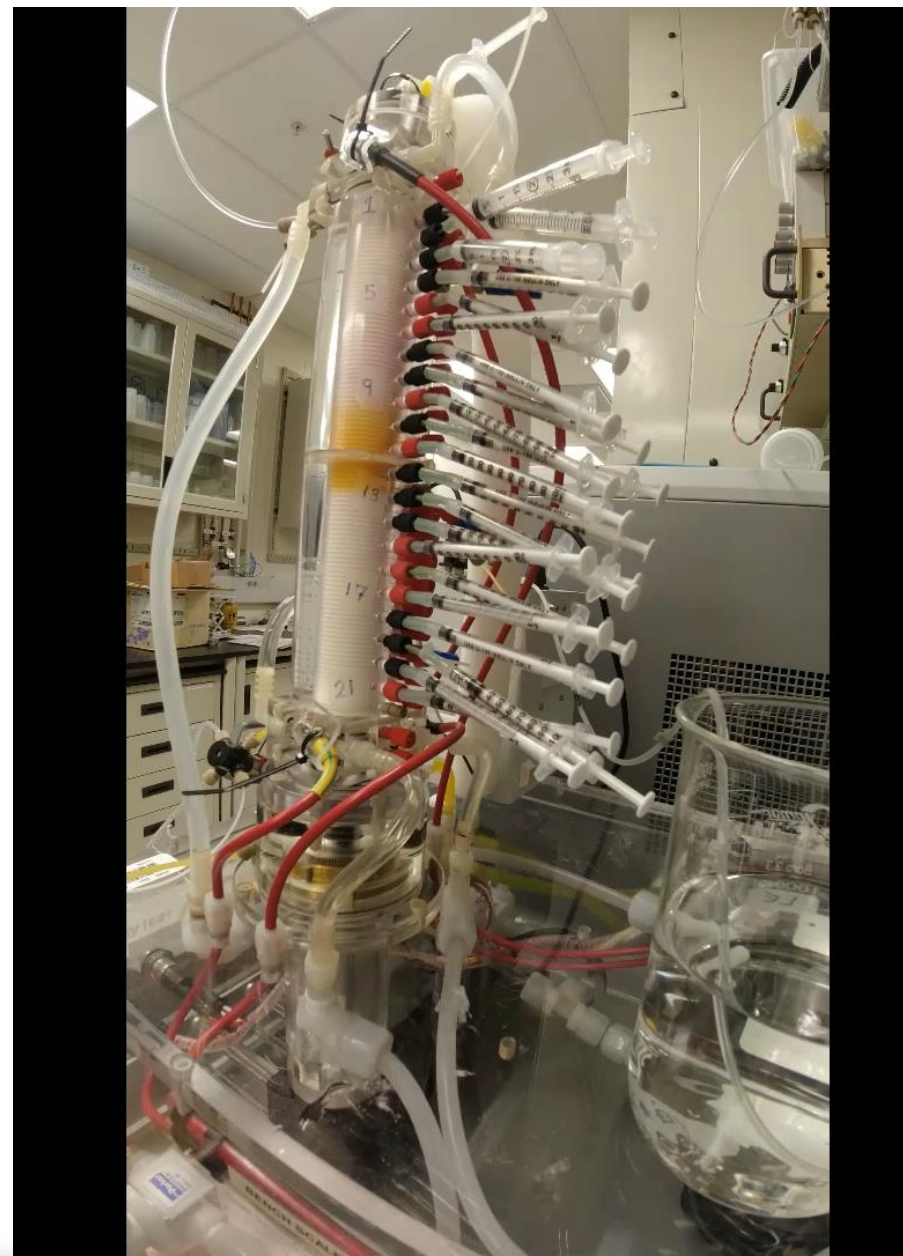
For ITP to work need a faster ion than Cl act as LE





# Initial testing – Moving Bed Electrophoresis

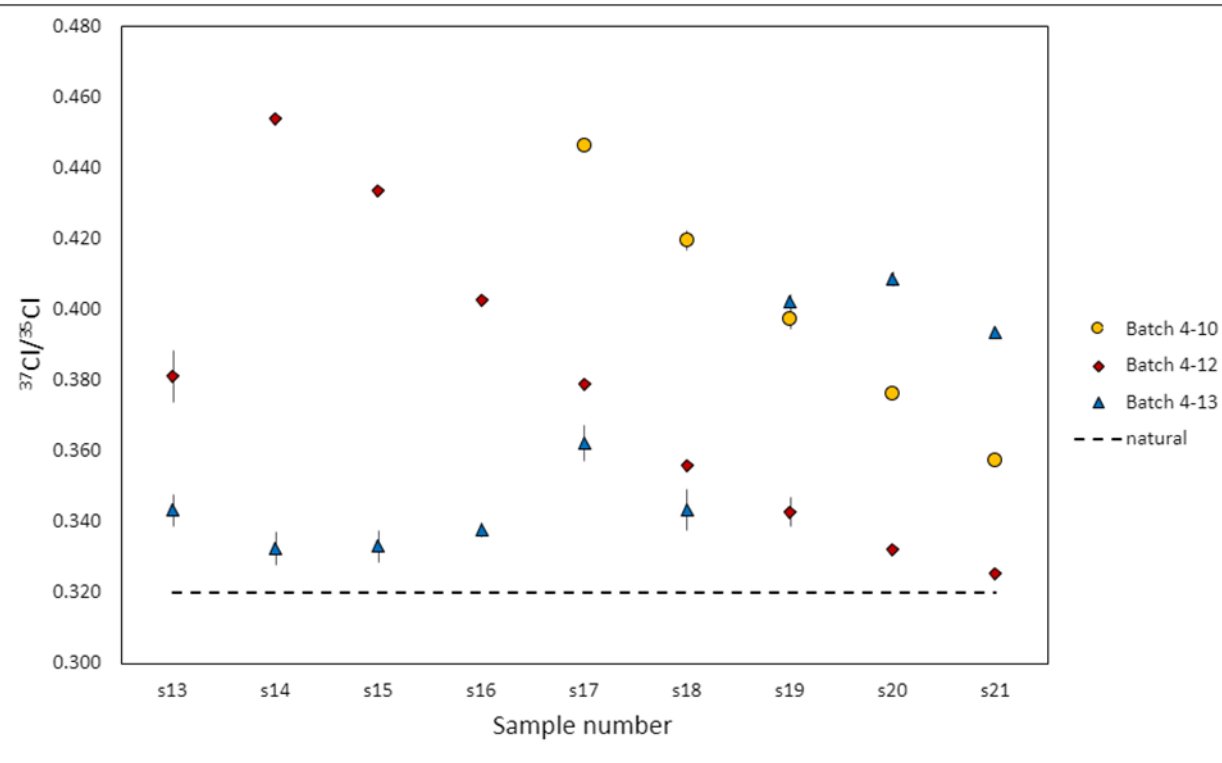
- Similar to ITP
  - Instead of LE you use sample as leading zone and slower ion, in this case,  $^{37}\text{Cl}$  will be enriched at TE interface
- ITP System
  - LE – 10mM HCl titrated to pH 8.8 with Tris
  - TE – 60 mM  $\epsilon$ -Aminocaproic acid (EACA) titrated to pH 9.5 with EACA
  - Sample – 0.4 mM Orange G used as a visual indicator to balance “upflow” counter flow with electric field



# Analytical Results from QQQ-ICPMS

- This is about what we expected in terms of enrichment based on previous results
  - Dispersion is the primary source of low enrichment levels
- Unexpected – samples close to the visible dye did not contain sufficient amount of chlorine to get an accurate measurement
  - Unknown – best guess currently is another anion contamination forming a zone between Cl-37 and visible dye
- Single stage separation factor ( $\alpha$ ):

$$\alpha = \frac{Cl37_{product} \cdot (1 - Cl37_{tails})}{Cl37_{tails} \cdot (1 - Cl37_{product})} = 1.81$$



Experiment	Experimental System	Voltage (kV)	Time (hr)	Meaningful Sample Numbers†
Batch 4-10	10mM HCl pH 8.8 w/ Tris	4.0	16	S17-S21
Batch 4-12	10mM HCl pH 8.64 w/ Tris	4.0	22	S14-S21
Batch 4-13	10mM HCl pH 8.8 w/ Tris	3.5	24	S19-S21
Batch 4-19*	10mM HCl pH 9.4 w/ Tris	3.5	24	*

\*Awaiting Results; †Samples that had sufficient counts to be reliable in their measurement.

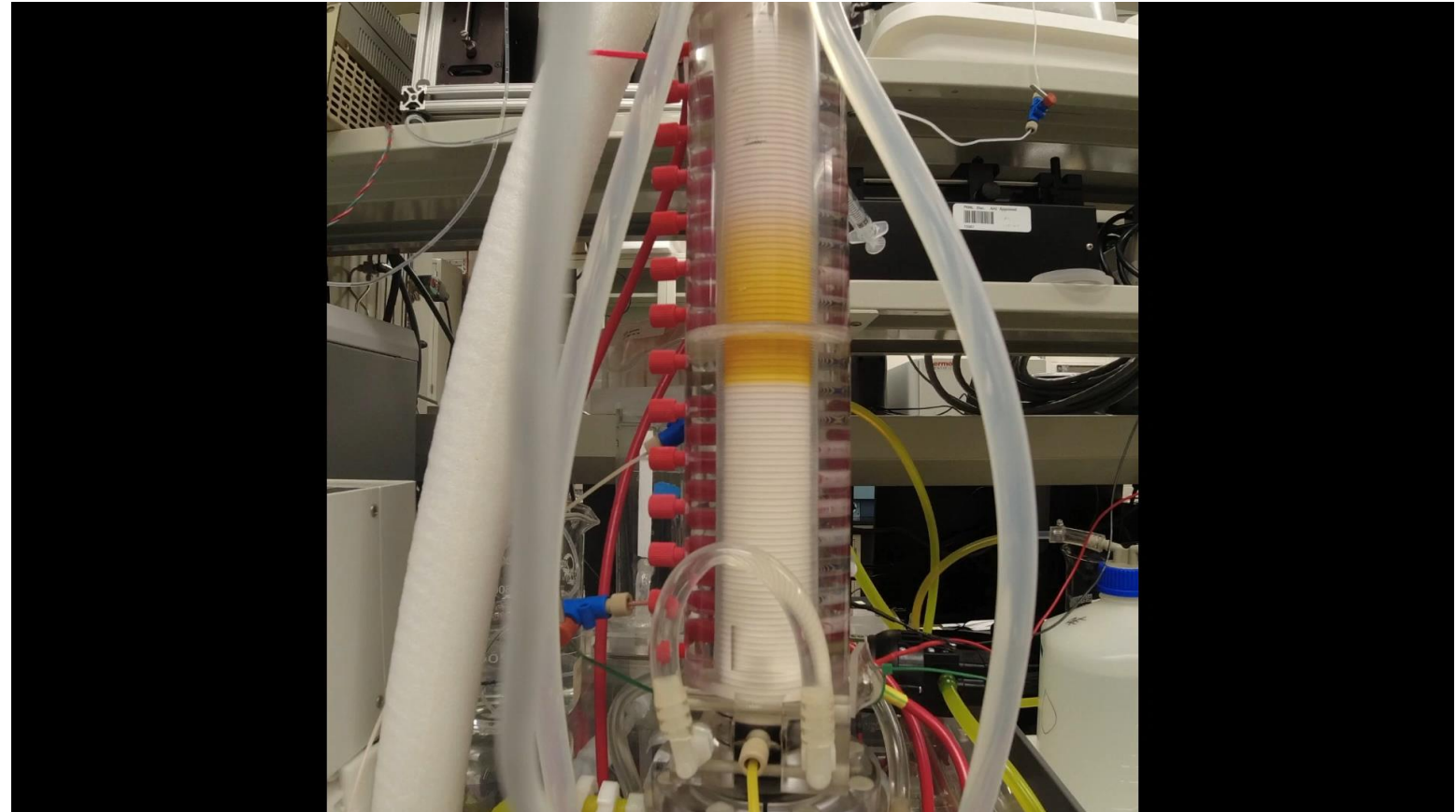
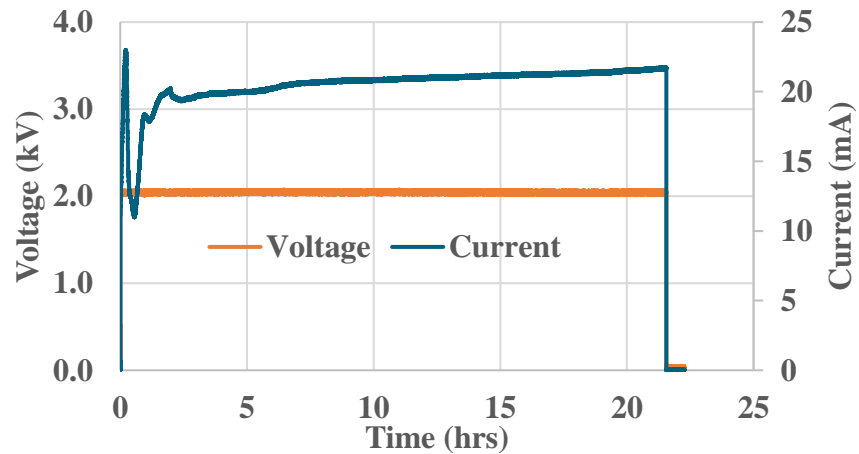


Expected to have Cl

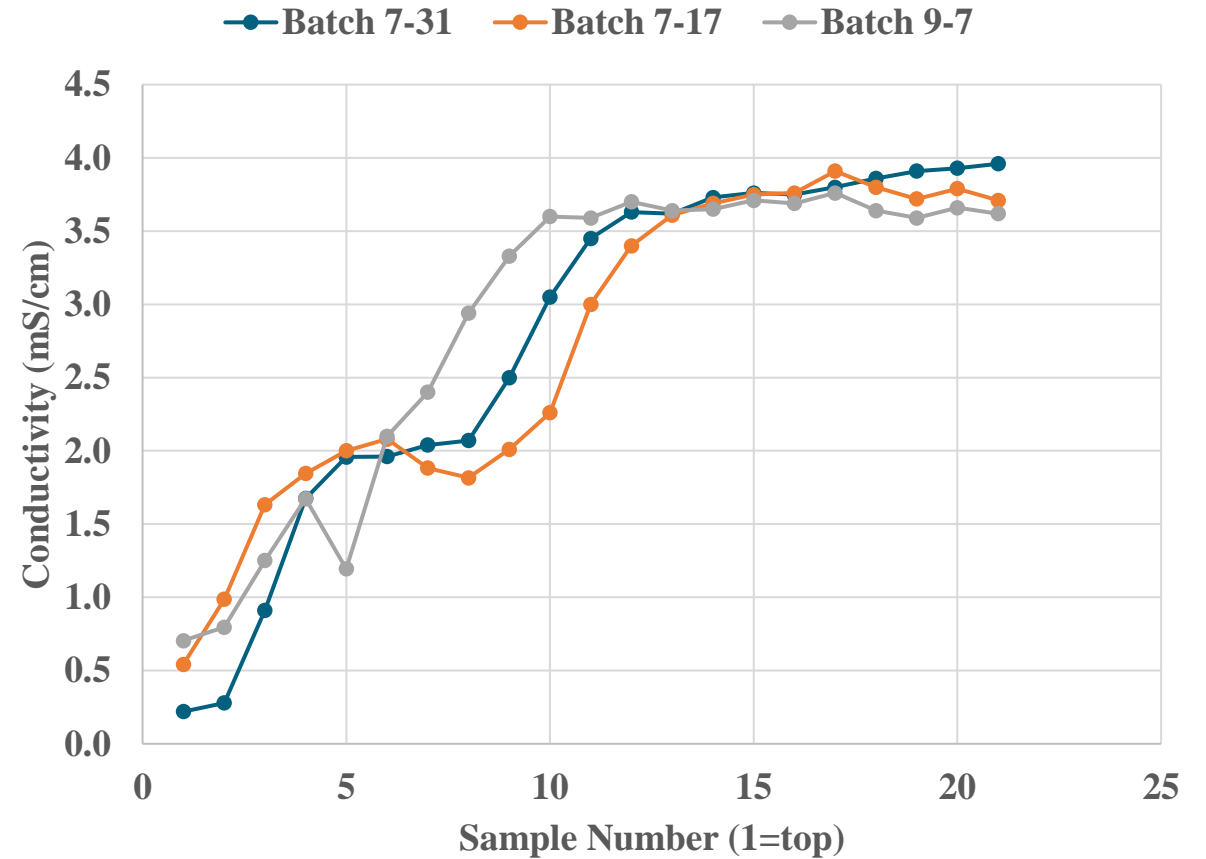
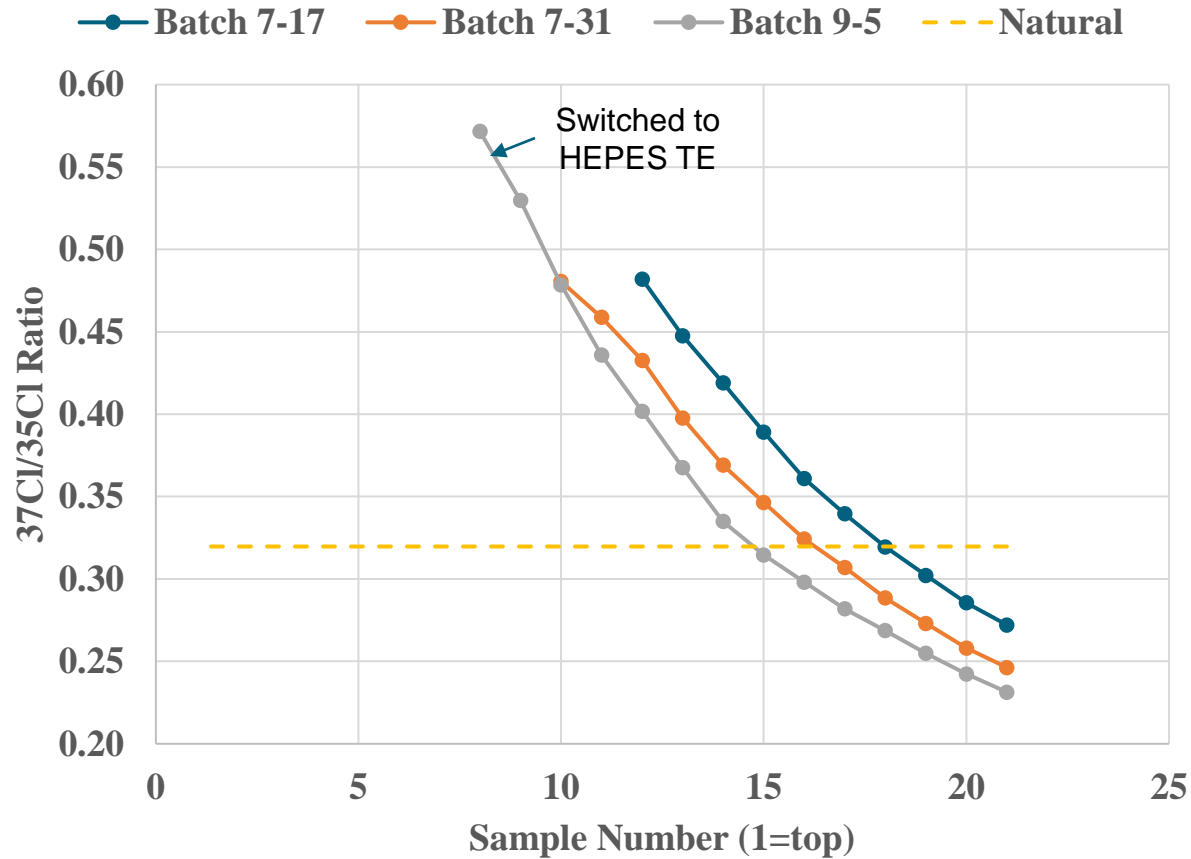
24 hr

# Isotachopheresis Demonstration

- LE: 10mM Ammonium Thiosulfate pH 9.3 with Ammonium Hydroxide
- TE: 10mM  $\epsilon$ -Aminocaproic Acid, 5mM barium hydroxide, pH 11.2
- Sample: 0.4mM Orange G Dye + 60mM Potassium Chloride in 3mL of TE

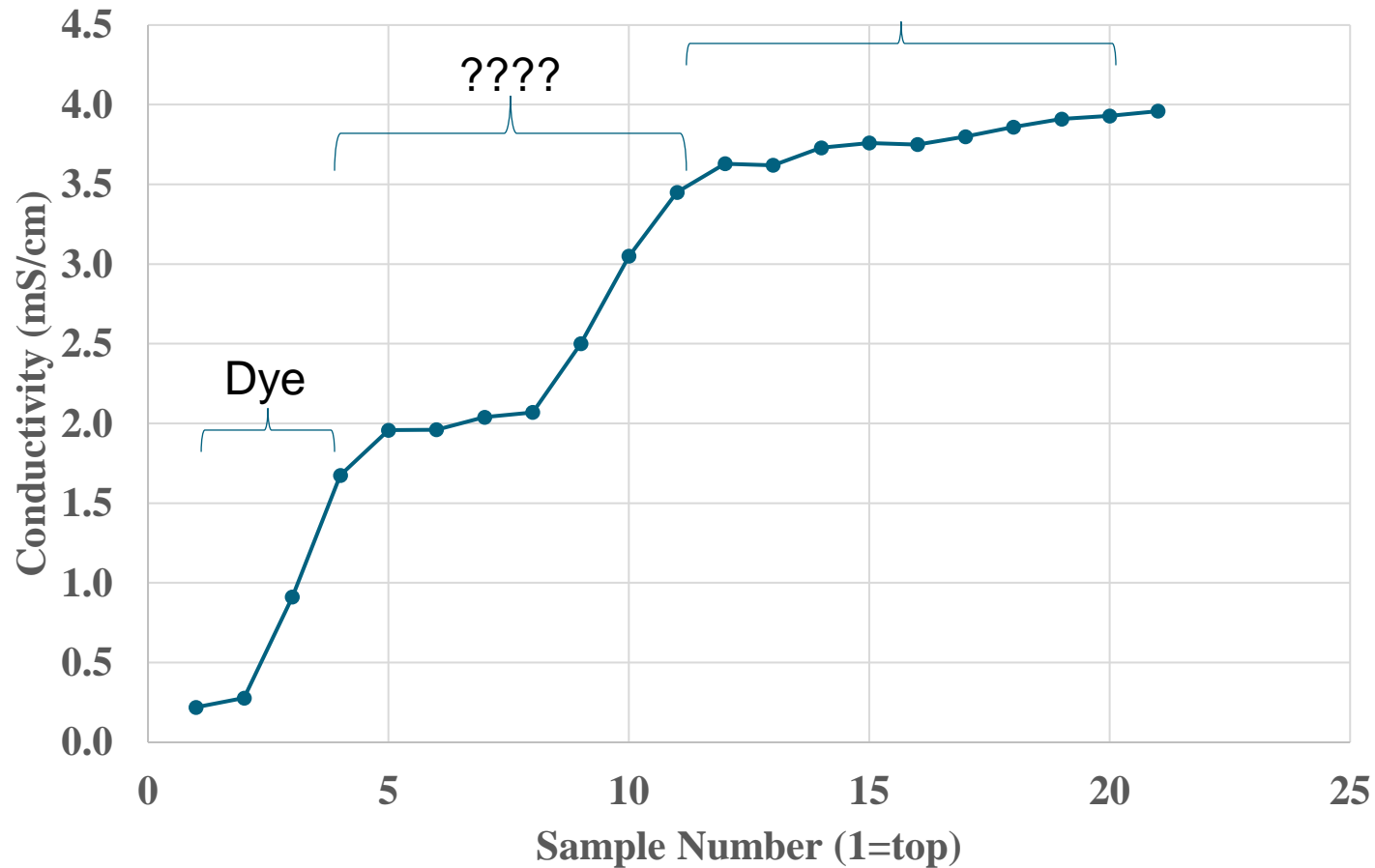


# Experimental Results



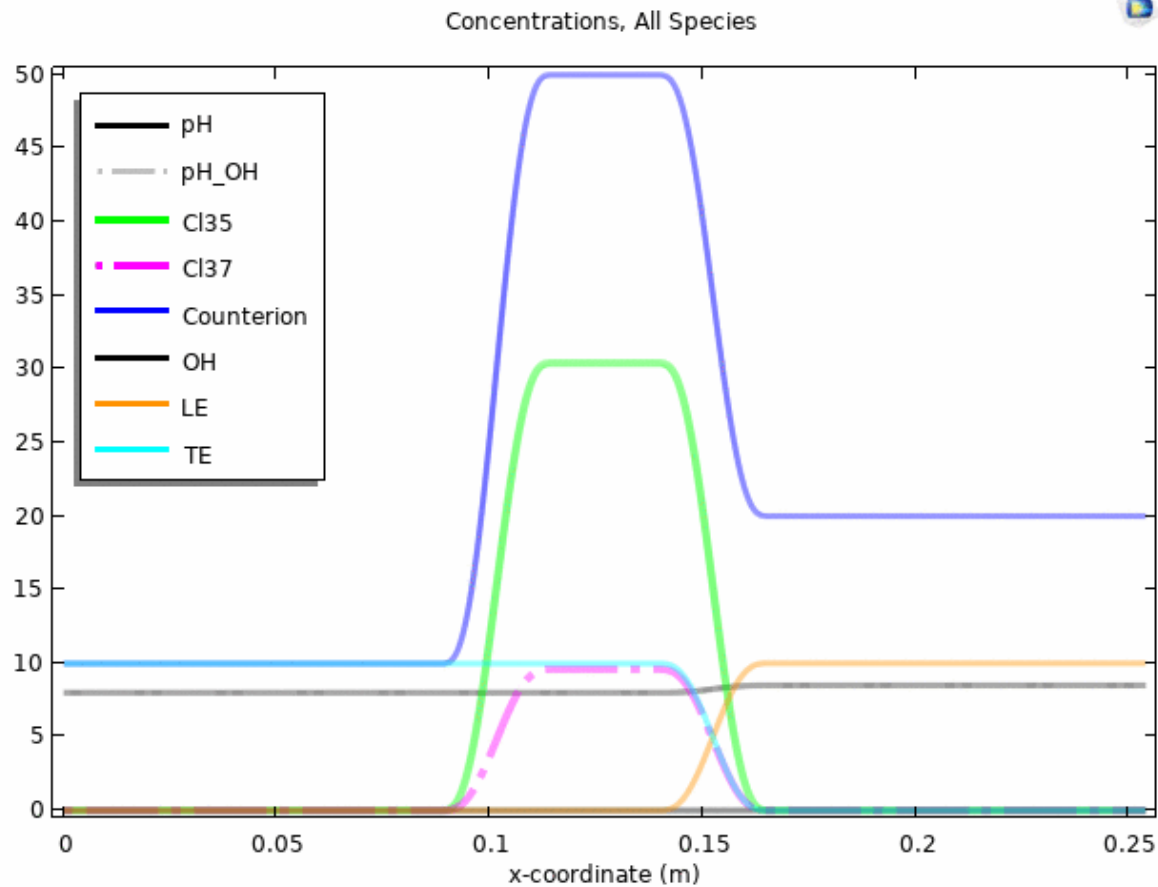
# Conductivity of Samples

Chloride



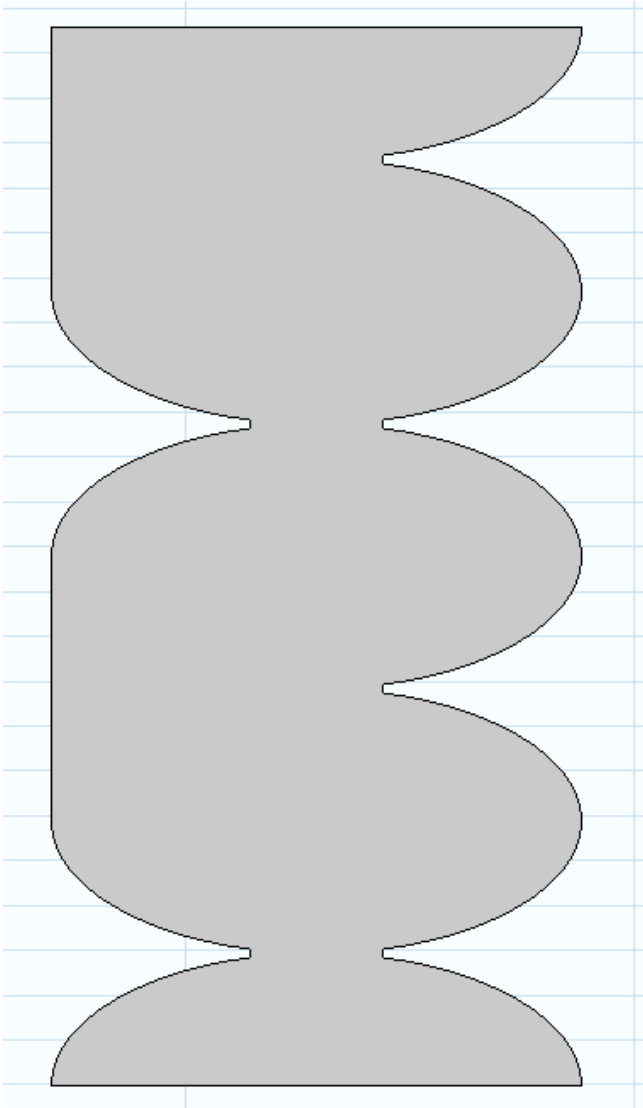
- Possibilities:
  - $\text{CO}_2$  dissolved in water  $\rightarrow$  carbonate or carbamate zones  $\rightarrow \text{Ba}(\text{OH})_2$
  - Nonvisible form of dye
  - Thiosulfate + Cl  $\rightarrow$  Bisulfate
  - TE has multiple forms  $\rightarrow$  Run with different TE
  - Some other contaminant???

# Numerical Simulation



- Indicates a ratio close to 1 after 24 hours
- Deep dive into experimental system and simulation results
- Current in simulation appears to be a factor of 6 higher than what is measured experimentally for this electrolyte system

# Geometric Tortuosity



- Shaping of VpHor rotor and stator has an impact on effective electric field.
- Experiments using 10 mM NaCl in 18 M $\Omega$  water yielded a tortuosity of about 2 in order to match the current between simulation and experiment.
- However, in ITP experiments a tortuosity of 6 was needed to get good agreement with the current between experiment and simulation.
- Depending on the electrolyte system we get a different number for the tortuosity indicating that its not a mechanical or geometric issue.

# Further Evidence

$$\mu_{\text{thiosulfate}} := 85 \cdot 10^{-9} \frac{\text{m}^2}{\text{V} \cdot \text{sec}}$$

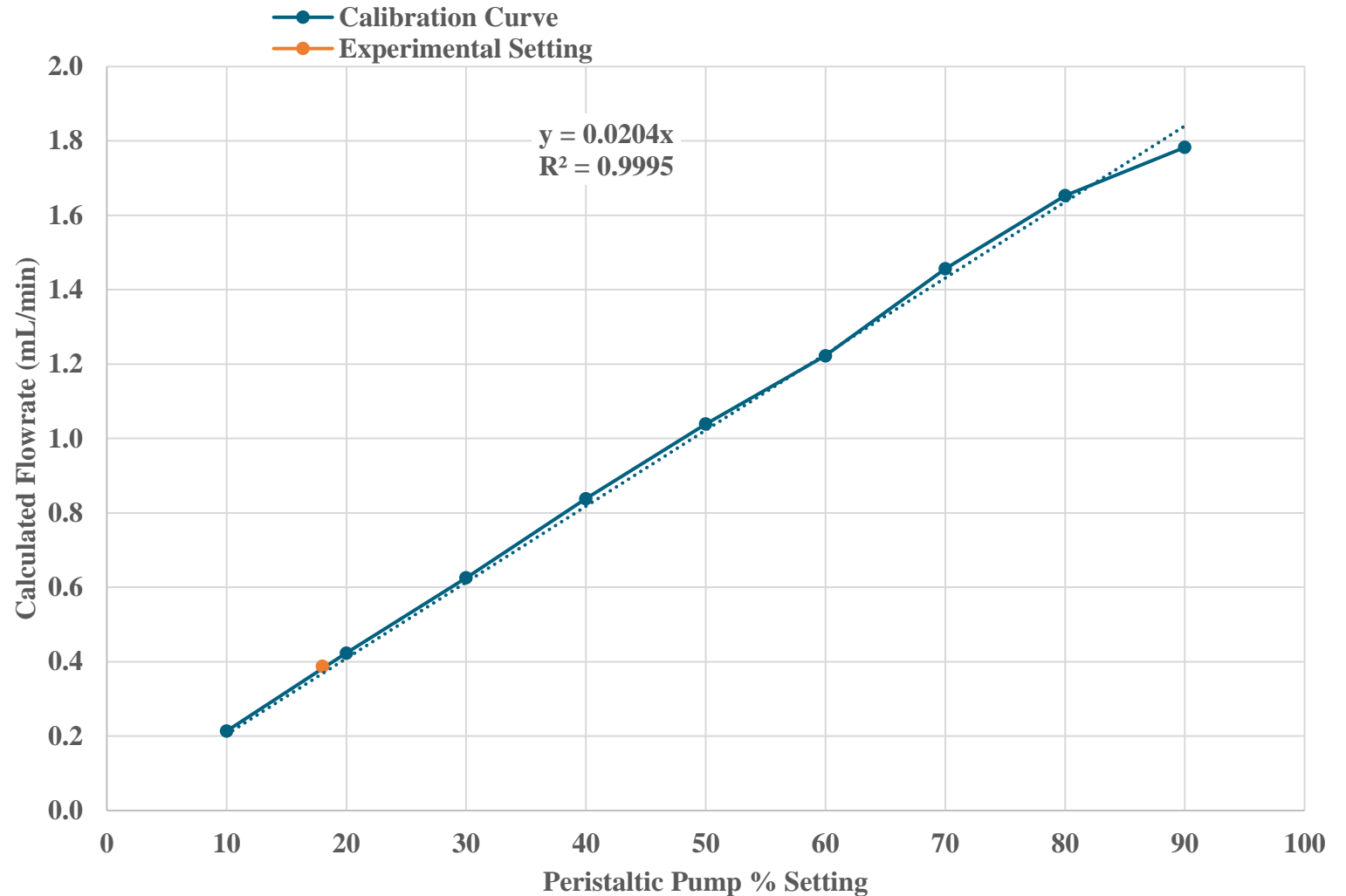
$$\text{length} := 30 \text{cm}$$

$$\text{CSA} := 0.685 \text{cm}^2$$

$$\text{tortuosity} := 6$$

$$\text{voltage} := \frac{2 \text{kV}}{\text{tortuosity}}$$

$$\text{velocity} := \frac{\text{voltage}}{\text{length}} \cdot \mu_{\text{thiosulfate}} \cdot \text{CSA} = 0.388 \cdot \frac{\text{mL}}{\text{min}}$$



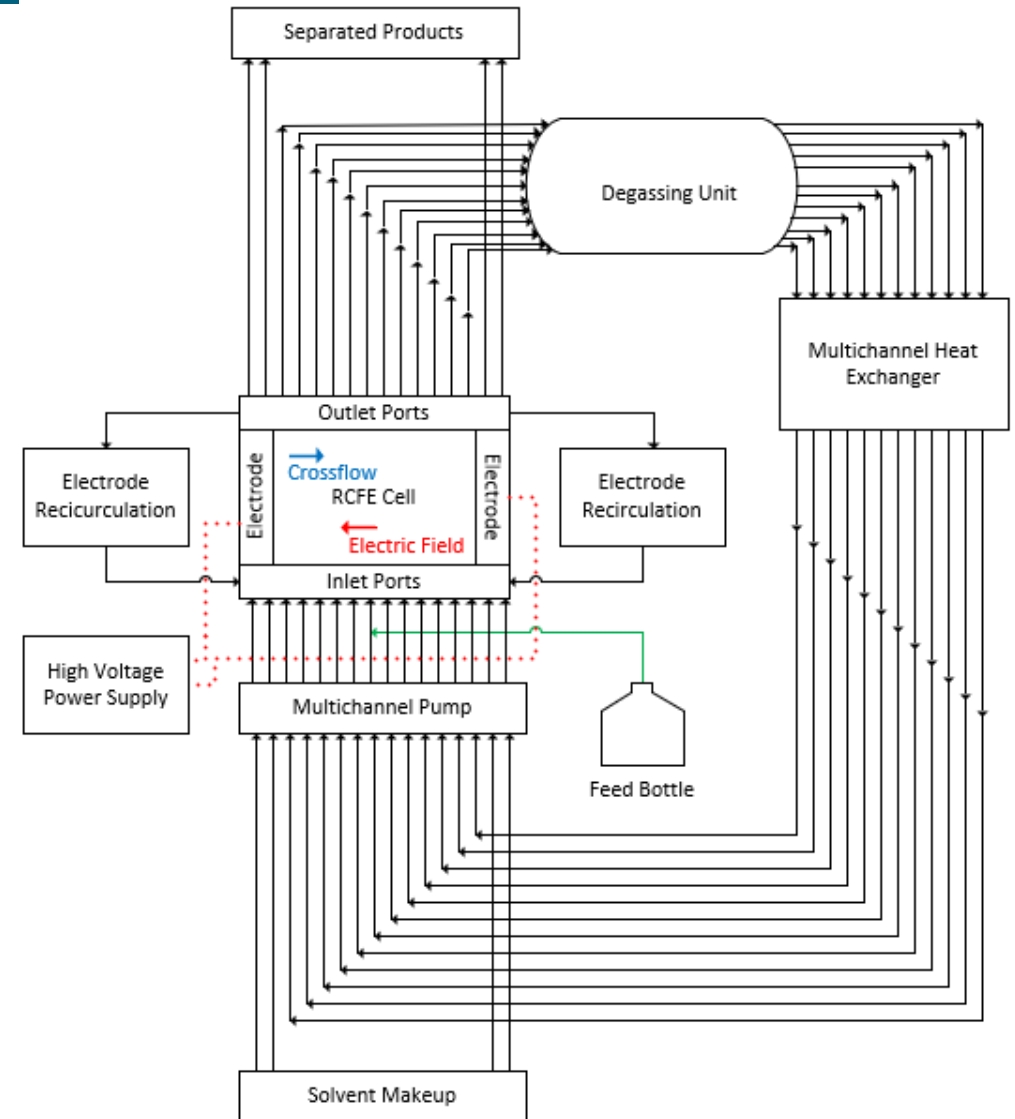


# Things to Keep in Mind

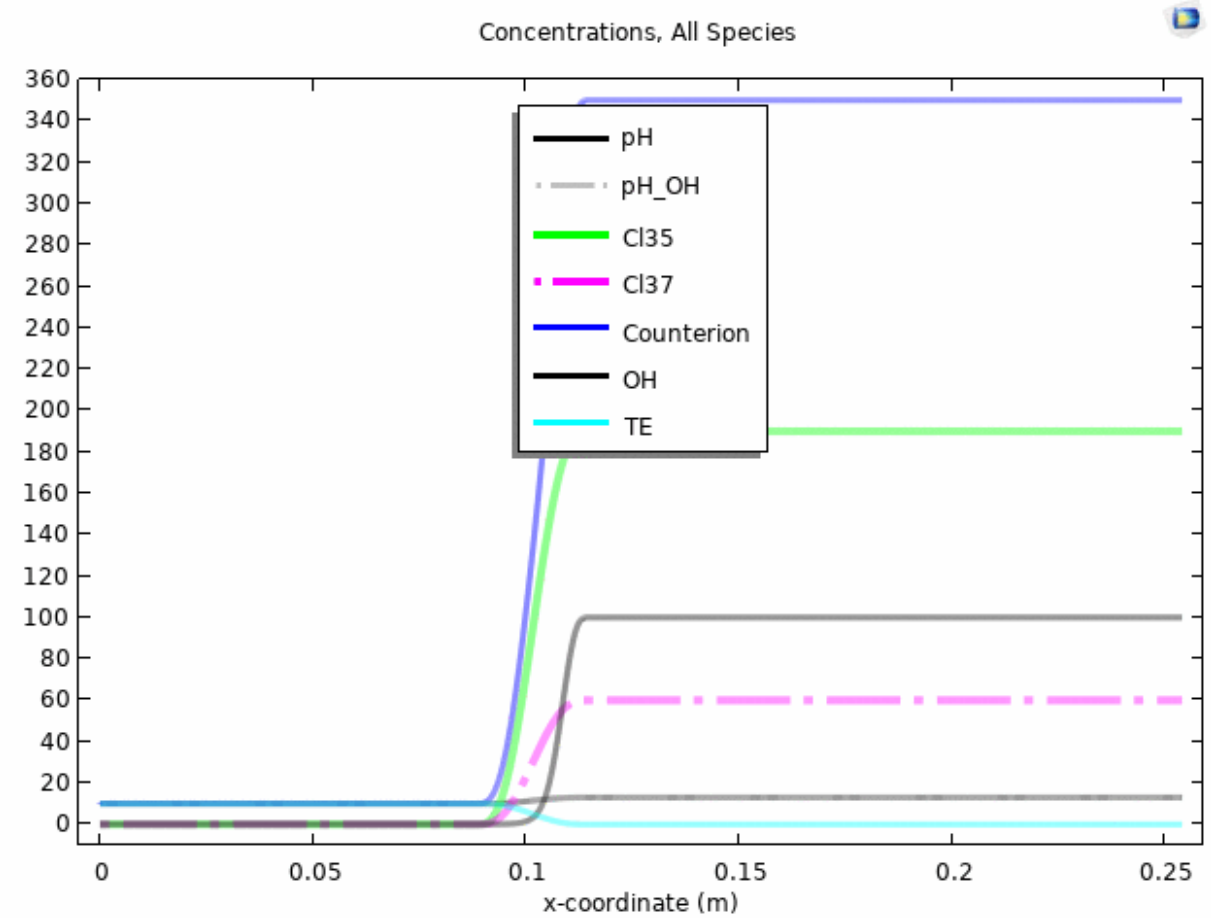
- Each decade increase in pH increases throughput by 10x
- ITP/MBE are expected to fail at  $\text{pH} > 13$
- Operation at higher pH will require better cooling due to the generation of Joule heat
- **Reduction of machine dispersion by 4x will dramatically increase enrichment as illustrated by the recycling continuous flow electrophoresis (RCFE) system**
- **It would be difficult to reduce dispersion in the existing electrophoresis unit but relatively easy to do this in the Flat-Bed RCFE by using surface coatings and adjusting the counterflow**

# Scale-Up and Design of New Electrophoresis System

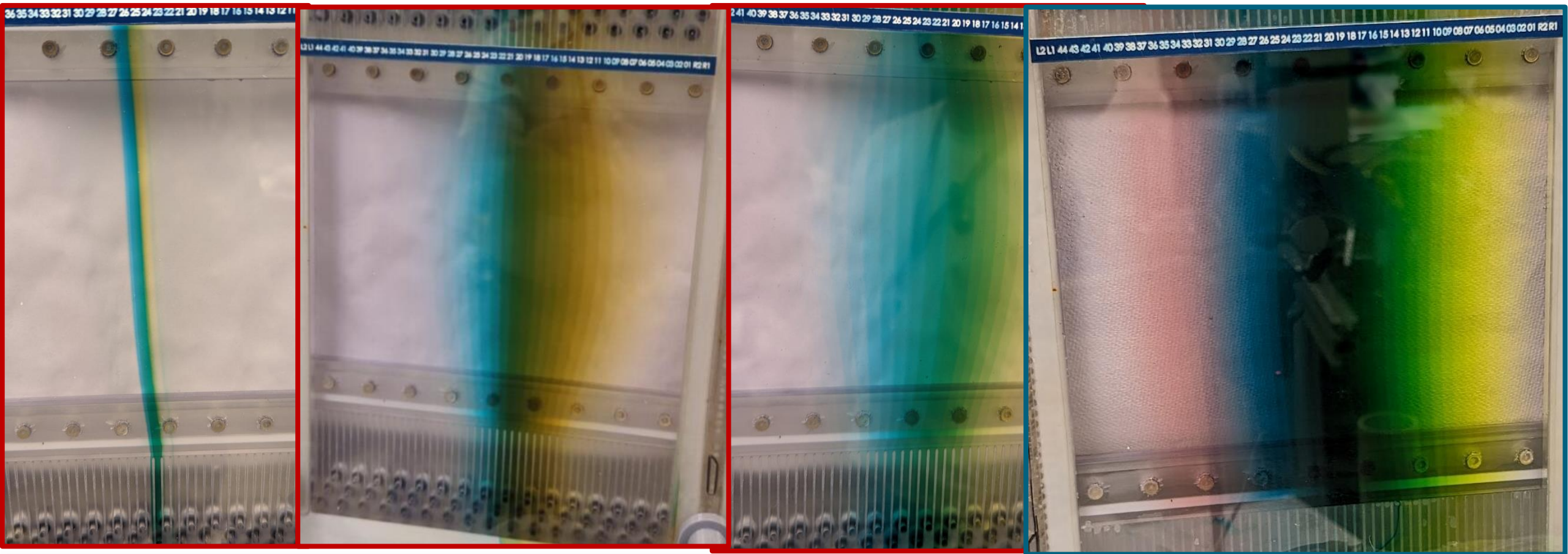
- Flat-Bed Recycling Continuous Flow Electrophoresis Device
- Two 24 Channel Peristaltic Pumps that Recycle Flow through the Device
- Degassing Unit to Remove Bubbles from System
- Heat Exchanger to Cool Fluid
- Electric Field from Right to Left
- Cross Flow from Left to Right
- Channel is 1 mm gap between Front Plate and Back Plate



# Constructed Test Stand



# Shakedown Experiments with Food Coloring



# Conclusions

- **Developed a capability for PNNL to quantify isotopic ratio of chlorine**
- **Demonstrated enrichment in state-of-the-art bench scale electrophoresis equipment despite higher than desirable dispersion**
  - Investigation into high dispersion presents need for Recycling Continuous Flow Electrophoresis Device
- **Developed new electrophoresis equipment design, i.e. RCFE**
  - Proof-of-concept shakedown with dye testing



# Thank you

[danny.bottenus@pnnl.gov](mailto:danny.bottenus@pnnl.gov)  
[shirmir.branch@pnnl.gov](mailto:shirmir.branch@pnnl.gov)

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